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(54) **SLEEVE MOLDING**

FORMEN EINER HÜLSE

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Description

[0001] The present invention relates to a method and apparatus for making multilayer injection-molded plastic articles such as preforms, wherein the successive molding of an inner sleeve and outer layer enables cost-effective production of multilayer preforms for pasteurizable, hot-fillable, and returnable and refillable beverage containers.

[0002] There is described in US-A- 4,609,516 to Krishnakumar et al. a method for forming multilayer preforms in a single injection mold cavity. In that method, successive injections of different thermoplastic materials are made into the bottom of the mold cavity. The materials flow upwardly to fill the cavity and form for example a five-layer structure across the sidewall. This five-layer structure can be made with either two materials (i.e., the first and third injected materials are the same) or three materials (i.e., the first and third injected materials are different). Both structures are in widespread commercial use for beverage and other food containers.

[0003] An example of a two-material, five-layer (2M, 5L) structure has inner, outer and core layers of virgin polyethylene terephthalate (PET), and intermediate barrier layers of ethylene vinyl alcohol (EVOH). An example of a three-material, five-layer (3M, 5L) structure has inner and outer layers of virgin PET, intermediate barrier layers of EVOH, and a core layer of recycled or post-consumer polyethylene terephthalate (PC-PET). Two reasons for the commercial success of these containers are that: (1) the amount of relatively expensive barrier material (e.g., EVOH) can be minimized by providing very thin intermediate layers; and (2) the container resists delamination of the layers without the use of adhesives to bond the dissimilar materials. Also, by utilizing PC-PET in the core layer, the cost of each container can be reduced without a significant change in performance.

[0004] Although the above five-layer, and other three-layer (see for example US-A-4,923,723) structures work well for a variety of containers, as additional high-performance and expensive materials become available there is an ongoing need for processes which enable close control over the amount of materials used in a given container structure. For example, polyethylene naphthalate (PEN) is a desirable polyester for use in blow-molded containers. PEN has an oxygen barrier capability about five times that of PET, and a higher heat stability temperature – about 250°F (120°C) for PEN, compared to about 175°F (80°C) for PET. These properties make PEN useful for the storage of oxygen-sensitive products (e.g., food, cosmetics, and pharmaceuticals), and/or for use in containers subject to high temperatures (e.g., refill or hot-fill containers). However, PEN is substantially more expensive than PET and has different processing requirements: Thus, at present the commercial use of PEN is limited.

[0005] Another high-temperature application is pasteurization – a pasteurizable container is filled and sealed at room temperature, and then exposed to an elevated temperature bath for about ten minutes or longer. The pasteurization process initially imposes high temperatures and positive internal pressures, followed by a cooling process which creates a vacuum in the container. Throughout these procedures, the sealed container must resist deformation so as to remain acceptable in appearance, within a designated volume tolerance, and without leakage. In particular, the threaded neck finish must resist deformation which would prevent a complete seal.

[0006] A number of methods have been proposed for strengthening the neck finish. One approach is to add an additional manufacturing step whereby the neck finish, of the preform or container, is exposed to a heating element and thermally crystallized. However, this creates several problems. During crystallization, the polymer density increases, which produces a volume decrease; therefore, in order to obtain a desired neck finish dimension, the as-molded dimension must be larger than the final (crystallized) dimension. It is thus difficult to achieve close dimensional tolerances and, in general, the variability of the critical neck finish dimensions after crystallization are approximately twice that prior to crystallization. Another detriment is the increased cost of the additional processing step, as it requires both time and the application of energy (heat). The cost of producing a container is very important because of competitive pressures and is tightly controlled.

[0007] An alternative method of strengthening the neck finish is to crystallize select portions thereof, such as the top sealing surface and flange. Again, this requires an additional heating step. Another alternative is to use a high T_g material in one or more layers of the neck finish. This also involves more complex injection molding procedures and apparatus.

[0008] Thus, it would be desirable to provide an injection-molded article such as a preform which incorporates certain high-performance materials, and a commercially acceptable method of manufacturing the same.

[0009] FR-A-2538297 to Aoki describes a two-step molding process, wherein a full-length inner sleeve of PET is formed in a first molding step on a first core, and the core and sleeve are transferred to a second cavity where a full-length outer layer of polycarbonate is molded over the sleeve. Aoki is directed to providing a specific molding apparatus in which a plurality of neck molds are mounted for rotational movement on a rotating platen, and a pair of injection cores are disposed for rotational movement above inner and outer molding stations, so that one of the injection cores is disposed above that portion of the rotating platen which is in line with the stopping position at the neck mold so that one of the injection cores can pass through one of the neck molds before it is inserted into the inner molding station.

[0010] GB-A-142956 to Bonis describes a two-step molding process, wherein a full-length inner sleeve is formed in a first molding step on a first core, and the core and sleeve are transferred to a second cavity where a full-length outer

layer is molded over the sleeve.

[0011] JP-5-73568 to Mitsubishi describes a two-step molding process, wherein a full-length inner sleeve of PET is formed at a first molding step on a first core, and the core and sleeve are transferred to a second cavity where a full-length outer layer of a mixture of PET and gas barrier resin is molded over the sleeve. Mitsubishi describes a specific process having a very long processing time, i.e., the inner layer is formed of a high copolymer which is processed for 30 minutes in order to increase the density. The outer layer includes a gas barrier polymer mixed with PET in order to improve the adhesion with the inner PET layer.

[0012] The present invention is directed to a method and apparatus for making a multilayer injection-molded plastic article, such as a preform, which is both cost-effective and enables control over the amounts of materials used in the various layers and/or portions of the article.

[0013] The present invention accordingly provides a method of reducing the inner layer thickness and improving the layer adhesion in a multiplayer injection-molded plastic article, the method comprising:

molding an inner sleeve layer between a first mold cavity and core, the first mold cavity being heated to maintain an outer surface of the inner sleeve layer at an elevated temperature;

transferring the core and sleeve layer to a second mold cavity and molding an outer layer over the sleeve layer while the outer surface is at the elevated temperature, the outer layer having a thickness greater than the thickness of the inner sleeve layer, where the elevated temperature is selected to provide melt adhesion between the inner sleeve and the outer layer during the second molding step.

[0014] According to a method/embodiment of the invention, an inner sleeve is molded on a first core positioned in a first mold cavity. The inner sleeve is only partially cooled before being transferred while still at an elevated temperature to a second mold cavity where an outer layer is molded over the inner sleeve. By providing the inner sleeve in the second mold cavity at the elevated temperature, bonding between the inner sleeve and outer layer is enabled during the second molding step, such that layer separation is avoided in the final molded article. The inner sleeve may comprise a full-length inner sleeve, extending substantially the full length of the article, or alternatively may comprise only an upper portion of the article, in which case the outer layer comprises a lower portion of the article and there is some intermediate portion in which the outer layer is bonded to the inner sleeve.

[0015] In one embodiment, a first thermoplastic material is used to make an inner sleeve which comprises a neck finish portion of the preform. The first thermoplastic material is preferably a thermal resistant material having a relatively high T_g , and/or forms a crystallized neck finish during the first molding step. In contrast, a lower body portion of the preform is made of a second thermoplastic material having a relatively lower thermal resistance and/or lower crystallization rate compared to the first material, and forms a substantially amorphous body-forming portion of the preform. In one example, by achieving crystallization in the neck finish during the first molding step, the initial and finish dimensions are the same so that the dimensional variations caused by the prior art post-molding crystallization step (and the expense thereof) are eliminated. Also, a higher average level of crystallization can be achieved in the finish, by utilizing the higher melt temperatures and/or elevated pressures of the molding process.

[0016] In another embodiment, a full-length body sleeve is provided made of a high-performance thermoplastic resin, such as PEN homopolymer, copolymer or blend. The PEN inner sleeve provides enhanced thermal stability and reduced flavor absorption, both of which are useful in refill applications. The amount of PEN used is minimized by this process which enables production of a very thin inner sleeve layer, compared to a relatively thick outer layer (made of one or more lower-performance resins).

[0017] Another aspect of the invention is an apparatus for the cost-effective manufacture of such preforms.

[0018] The present invention accordingly further provides an apparatus for making multiplayer injection-molded plastic articles comprising:

a first mold cavity set and a second mold cavity set, each first cavity being adapted to form an inner sleeve layer and each second cavity being adapted to form an outer layer, the outer layer having a thickness greater than the thickness of the inner sleeve layer;

a transfer mechanism with first and second core sets for successively positioning the first and second core sets in the first and second cavity sets;

wherein the first core set is positionable in the first cavity set for molding a set of inner sleeve layers on the first core set, while the second core set is positionable in the second cavity set for molding, over a previously-molded set of inner sleeve layers on the second core set, a second set of outer layers; and

means for heating the first cavity set so as to maintain an outer surface of the inner sleeve layer at an elevated temperature during transfer and molding of the outer layer thereover, the elevated temperature being selected to provide melt adhesion between the inner sleeve and outer layer.

[0019] The apparatus includes at least one set of first and second molding cavities, the first mold cavity being adapted to form the inner sleeve and the second mold cavity adapted to form the outer layer. A transfer mechanism includes at least one set of first and second cores, wherein the cores are successively positionable in the first and second molding cavities. In one cycle, a first core is positioned in a first mold cavity while a first inner sleeve is molded on the first core, while a second core, carrying a previously-molded second inner sleeve, is positioned in a second mold cavity, for molding a second outer layer over the second inner sleeve. By simultaneously molding in two sets of cavities, an efficient process is provided. By molding different portions/layers of the articles separately in different cavities, different temperatures and/or pressures may be used to obtain different molding conditions and thus different properties in the different portions/layers. For example, it is possible to mold the crystallized neck finish portion in a first cavity, while molding a substantially amorphous outer layer in the second cavity.

[0020] The resulting injection-molded articles, and/or expanded injection-molded articles, may thus have a layer structure which is not obtainable with prior processes.

[0021] The following chart provides temperature/time/pressure ranges for certain preferred embodiments, which are described in greater detail in the following sections:

a) for an inner sleeve of PEN polymer material and an outer layer of PET polymer material

first molding step:	range (on the order of)
core temperature	5-80°C
mold cavity temperature	40-120°C
melt temperature	275-310°C
cycle time	4-8 seconds
outer surface temperature of sleeve	60-120°C
second molding step:	
core temperature	5-80°C
mold cavity temperature	5-60°C
cycle time	20-50 seconds
pressure	$55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi)

b) for an inner sleeve of crystallized polyester material and an outer layer of PET polymer material

first molding step:	range (on the order of)
core temperature	5-60°C
mold cavity temperature	80-150°C
melt temperature	270-310°C
cycle time	5-8 seconds
outer surface temperature of sleeve	80-140°C
second molding step:	
core temperature	5-60°C
mold cavity temperature	5-60°C
cycle time	20-35 seconds
pressure	$55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi)

[0022] The present invention will be more particularly set forth in the following detailed description and accompanying drawings.

Figs. 1A-1D are schematic illustrations of a first method embodiment of the present invention for making a preform having a full-length inner sleeve and a single outer layer;

Figs. 2A-2B are schematic illustrations of an injection-molding apparatus and the sequence of operations for making a preform such as that shown in Fig. 1D, wherein a rotary turret transfers two sets of cores between two sets of cavities; Fig. 2A shows the cavities/cores in a closed position and Fig. 2B shows the cavities/cores in an open position;

Fig. 3 is a time line showing the sequence of operations for the molding apparatus of Fig. 2;

Fig. 4A is a front elevational view of a returnable and refillable container, partially in section, made from the preform of Fig. 1D, and Fig. 4B is an enlarged fragmentary cross-section of the container sidewall taken along the line 4B-4B of Fig. 4A;

Figs. 5A-5D are schematic illustrations of a second method embodiment of the present invention for making a preform having a finish only sleeve and a multilayer outer layer;

Figs. 6A-6D are schematic illustrations of an injection-molding apparatus and sequence of operations for making a preform such as that shown in Fig. 5D, wherein the transfer mechanism is a reciprocating shuttle; Fig. 6A shows the shuttle in a first closed position in first and second mold cavities; Fig. 6B shows the shuttle in a second open position after retraction from the first and second mold cavities; Fig. 6C shows the shuttle in a second open position beneath the second and third mold cavities; and Fig. 6D shows the shuttle in a fourth closed position in the second and third mold cavities;

Fig. 7 is a time line of the sequence of operations shown in Fig. 6;

Fig. 8A is a cross-sectional view of a third preform embodiment of the present invention having a full-thickness neck sleeve and multilayer body portion, and Fig. 8B is an enlarged fragmentary view of the neck finish of the preform of Fig. 8A;

Fig. 9A is a front elevational view of a hot-fill container made from the preform of Fig. 8A, and Fig. 9B is a fragmentary cross-section of the container sidewall taken along line 9B-9B of Fig. 9A;

Fig. 10 is a cross-sectional view of a fourth preform embodiment of the present invention, having a full-length body sleeve and multilayer outer layer;

Fig. 11 is a cross-sectional view of a fifth preform embodiment of the present invention, including a full-length body sleeve and an extra outer base layer;

Fig. 12 is a cross-sectional view of a sixth preform embodiment of the present invention, having a finish sleeve and a single layer outer layer;

Figs. 13A and 13B are graphs showing the change in melting temperature (MP) and orientation temperature (T_g) for various PEN/PET compositions; and

Fig. 14 is a schematic illustration of a three-station reheating apparatus, including IR heating stations A and C and RF heating station B.

First Preform Embodiment (refillable water)

[0023] Figs. 1A-1D illustrate schematically one method embodiment for making a preform with a full-length body sleeve and a single outer layer; this preform is particularly useful for making a returnable and refillable water bottle. Fig. 1A shows a first core 9 positioned in a first mold cavity 11, and forming a chamber therebetween in which there is formed an injection-molded inner sleeve 20. The sleeve 20 is partially cooled and then the core 9 carrying sleeve 20 is removed from the first mold cavity as shown in Fig. 1B. While still warm, the sleeve 20 on core 9 is inserted into a second mold cavity 12 which forms an interior molding chamber for forming an outer layer 22 over the inner sleeve 20. After the second molding step, a preform 30 has been formed including outer layer 22 and inner sleeve 20 as shown in Fig. 1D. The inner sleeve includes a top flange 21 which will form the top sealing surface of the resulting container (see Fig. 4).

[0024] The first method embodiment will now be described in greater detail in regard to the apparatus shown in Figs. 2A-2B, and a time sequence of operations illustrated in the time line of Fig. 3.

[0025] As shown in Figs. 2A-2B, a four-sided rotatable turret 2 is interposed between a fixed platen 3 and a movable platen 4 on an injection-molding machine. The turret 2 is mounted on a carriage 5 which is slidable in the direction of platen motion (shown by arrows A_1 and A_2). The turret 2 is rotatable (shown by arrow A_3) about an axis 6 disposed perpendicular to the direction of platen motion. The turret is rotatable into two operative positions spaced 180° apart. In each of these positions, the two opposing faces 7, 8 of the turret carrying first and second sets of cores 9, 10 respectively, are received in a first set of cavities 11 on the movable platen 4, and a second set of cavities 12 on the fixed platen 3. After a core set has been successfully positioned in each of the mold cavities, the finished preforms may be ejected from the cores. Each of the mold cavity and core sets include water passages 15 for heating or cooling of the cavities/cores to achieve a desired temperature during molding.

[0026] The sequence of operations for forming a particular preform will now be described. The preform has a full-body sleeve of a PEN polymer, such as homopolymer PEN, or a PEN/PET copolymer or blend. The preform has a single outer layer made of virgin PET.

[0027] In Fig. 2A, the movable platen 4 carrying the first set of mold cavities 11, and the carriage 5 carrying the turret 2, are each moved on guide bars (tie rods) 13, 14 to the left towards the fixed platen 3 to close the mold (i.e., both cavities). The first set of cores 9 on the left face 7 of the turret are positioned in the first cavity set 11 (first molding station); each first core/cavity pair defines an enclosed chamber for molding an inner sleeve about the first core. The

PEN polymer is injected via nozzle 16 into the first mold cavities to form the inner sleeve. Simultaneously, the second core set 10 (on the second face 8 of the turret) is positioned in the second cavity set 12 (second molding station). Virgin PET is injected via nozzle 17 into the second set of cavities to form a single outer layer about a previously-formed inner sleeve on each of the second cores.

5 **[0028]** Next, the mold is opened as shown in Fig. 2B by moving both the movable platen 4 and carriage 5 to the left, whereby the first cores 9 are removed from the first cavity 11 and the second cores 10 are removed from the second cavity 12. Now, the finished preforms 30 on the second core set are ejected. The finished preforms 30 may be ejected into a set of robot cooling tubes (not shown) as is well known in the art. Next, the turret 2 is rotated 180°, whereby the first set of cores 9 with the inner sleeves 20 thereon are now on the right side of the turret (and ready for insertion into the second set of cavities), while the second set of (empty) cores 10 is now on the left side of the turret (ready for insertion into the first set of mold cavities). Again, the mold is closed as shown in Fig. 2A and injection of the polymer materials into the first and second sets of cavities proceeds as previously described.

10 **[0029]** In this embodiment, the first and second cores are held at a temperature in a range on the order of 60-70°C, whether they are positioned in the first mold cavities or the second mold cavities. The first mold cavities (for forming the inner sleeve) are held at a temperature on the order of 85-95°C. The melt temperature of the PEN polymer is on the order of 285-295°C. The cycle time in the first mold cavity is on the order of 6-7 seconds, i.e., the time lapse between the first and second injections. This is because, as shown in Fig. 3, the hold and cool stage is substantially eliminated in the first mold cavities. The outer surface temperature of the sleeve (opposite the inner surface engaging the core) at the start of the second injection is 100-110°C.

20 **[0030]** During the second molding step, the core temperature is again at 60-70°C, but the second mold cavity temperature is 5-10°C (much lower than the first cavity temperature, to enable quick cooling of the preform). The melt temperature of the virgin PET is on the order of 260 to 275°C; this is lower than the melt temperature of the PEN polymer, but because the PEN polymer is still warm (at a temperature of 100-110°C) during the second molding step, there is melt adhesion (including diffusion bonding and chain entanglement) which occurs between the PEN polymer chains and virgin PET polymer chains (inner sleeve and outer layer) respectively. The cycle time for the second molding step is on the order of 35 to 37 seconds.

25 **[0031]** Fig. 3 is a time line with the cycle time along the x axis (time in seconds), and the sequence of steps in the second cavity set shown above the x axis, and the sequence of steps in the first cavity set shown below the x axis. At $t = 0$, the mold is closed (see Fig. 2A) and the pressure is built up. At $t = 1.5$ seconds, the second cavity (for forming the outer layer) is filled, the pressure boosted, and then the pressure reduced during the hold and cooling stage; this continues until $t = 33$ seconds in the second cavity. Meanwhile, no action is required at $t = 1.5$ seconds in the first cavity ("no action period"); rather, it is not until $t = 31$ seconds that the first cavity is filled and the pressure increased and held, until $t = 33$ seconds. This substantial elimination of the hold and cooling stage (in the first cavity) produces an inner sleeve which is still at an elevated temperature when it is subsequently positioned in the second cavity, and enables melt adhesion between the outer surface of the inner sleeve and outer layer. At $t = 33$ seconds, the mold is opened (see Fig. 2B), and the preforms from the second cavity are ejected. Then, at $t = 35$ seconds, the turret 2 is rotated so as to position the still-warm sleeves (just made in the first cavity) in a position to be inserted into the second cavity, while the now-empty core set (previously in the second cavity) is now positioned to be inserted in the first cavity. At $t = 36$ seconds, we are ready to begin the next cycle.

30 **[0032]** The method and apparatus of Fig. 2 may be advantageously used to produce multilayer preforms for a great variety of applications, including refill, hot-fill and pasteurizable containers. A number of alternative embodiments are described below.

35 **[0033]** The preform made according to the method and apparatus of Figs. 1-3 includes a full-body inner sleeve 20 of PEN polymer, and a single outer layer 22 of virgin PET. The preform is substantially transparent and amorphous and may be reheated and stretch blow-molded to form a 1.5 liter returnable and refillable water bottle, such as that shown in Fig. 4A. The container 40 is about 13.2 inches (335 mm) in height and about 3.6 inches (92 mm) in widest diameter. The container body has an open top end with a small diameter neck finish 42 having external screw threads for receiving a screw cap (not shown), and a closed bottom end or base 48. Between the neck finish 42 and base 48 is a substantially vertically-disposed sidewall 45 (defined by vertical axis or centerline CL of the bottle), including a substantially cylindrical panel portion 46 and a shoulder portion 44 tapering in diameter from panel 45 to neck finish 42. The base 48 is a champagne-style base with a central gate portion 51 and, moving radially outwardly towards the sidewall, an outwardly concave dome 52, an inwardly concave chime 54, and a radially increasing and arcuate outer base portion 56 for a smooth transition to the sidewall panel 46. The chime 54 is a substantially toroidal-shaped area around a standing ring (chime) on which the bottle rests.

40 **[0034]** Fig. 4B shows in cross-section the multilayer panel portion 46, which includes an inner sleeve layer 41 (an expanded version of preform sleeve 20), and an outer layer 43 (an expanded version of preform outer layer 22). One benefit of the present invention is that the layers 41 and 43 have bonded and will not separate during reheat stretch blow molding or use of the container, in this case including the intended 20 or more refill cycles. In addition, a flange

47 (same as flange 21 of the preform) forms a top sealing surface of the container with increased strength and thermal resistance.

Second Preform Embodiment (pasteurizable beer)

[0035] Figs. 5A-5D illustrate schematically a second method embodiment for making a finish-only sleeve and a multiple outer layer preform; this preform is adapted for making a pasteurizable beer container. Fig. 5A shows a core 207 positioned in a first mold cavity 213; together they form a first molding chamber in which a finish-only sleeve 250 is injection molded. Fig. 5A shows an injection nozzle 211 in the mold cavity 213, through which a molten thermoplastic material is injected for forming the sleeve 250. Fig. 5B shows the formed sleeve 250 on the core 207, the sleeve having been removed from first mold cavity 213 while it is still warm. The core 207 carrying the sleeve 250 is then positioned in a second mold cavity 214 as shown in Fig. 5C. The second mold cavity 214 and core 207 form a second molding chamber adapted to form an outer layer 252 over the inner sleeve 250. A plurality of different thermoplastic materials are injected through a gate 209 in the bottom of the second mold cavity 214, to form the multiple outer layers. As shown in Fig. 5D, the outer layer 252 extends the full length of the preform. A sequential injection process such as that described in U.S. Patent No. 4,609,516 to Krishnakumar et al., may be used to form inner and outer layers 253, 254 of virgin PET, core layer 255 of recycled PET (which may include an oxygen scavenging material), and inner and outer intermediate layers 256, 257 of an oxygen barrier material, between the inner/core/outer layers. In this embodiment, only the virgin PET extends up into the neck finish of the preform, forming a single layer 258 over inner sleeve 250. In the base of the preform, a final injection of virgin PET forms a plug 259 for clearing the nozzle before the next injection cycle.

[0036] Figs. 6A-6D illustrate a reciprocating shuttle apparatus, instead of the rotatable turret of Figs. 2A-2D, which comprises a second apparatus embodiment. This second apparatus will now be described with respect to forming the preform of Fig. 5. Fig. 7 shows a time line of the sequence of operations.

[0037] The apparatus (see Figs. 6A-6D) includes first and second parallel guide bars 202, 203 on which a platen 205 is movably mounted in the direction of arrow A_4 . The platen 205 carries a platform or shuttle 206 which is movable in a transverse direction across the platen 205 as shown by arrow A_5 . A fixed platen 212 at one end of the guide bars holds three injection mold cavity sets 213, 214 and 215 which are supplied by nozzles 218, 219 and 220 respectively. The left (first) and right (third) cavity sets 213 and 215 are used to form neck portions of preforms, while the middle (second) cavity set 214 is used for molding body-forming portions.

[0038] Fig. 5A shows an arbitrarily-designated first step wherein the first core set 207 is positioned in left cavity set 213 for forming a first set of preform neck portions (sleeves). Simultaneously, second core set 208 is positioned in middle cavity set 214 for molding a set of multilayer body-forming portions (over a second set of previously molded neck portions). Fig. 5B shows the core sets following removal from the cavity sets, with a neck sleeve 250 on each core of core set 207, and a preform 260 on each core of core set 208. The completed preforms 260 are then ejected from the core set 208.

[0039] In a second step (Fig. 6C), the shuttle 206 is moved to the right such that the first core set 207 with neck sleeves 250 are now positioned below middle cavity 214, while second core set 208 with now empty cores 216 is positioned below right cavity set 215. Movable platen 205 is then moved towards fixed platen 212 so as to position first core set 207 in middle cavity set 214, and second core set 208 in right cavity set 215 (Fig. 6D). Again, body-forming portions are formed over the previously formed neck sleeves in middle cavity set 214, while neck sleeves are molded on each of the cores in the core set 208 in right cavity set 215. The movable platen 205 is then retracted to remove the core sets from the cavity sets, the finished preforms on the first core set 207 are ejected, and the shuttle 206 returns to the left for molding the next set of layers.

[0040] Fig. 7 is a time line of the operations shown in Fig. 6, with time in seconds along the x axis, and the sequence of steps in the second cavity 214 shown above the x axis, and the sequence of steps in the first cavity 213 shown below the x axis. First, at $t = 0$, the mold is closed (Fig. 6A) and the pressure builds up. Then, at $t = 1.5$ seconds, the second cavity 214 is filled (forming the outer layer), the pressure increased, and the pressure held while the preform cools, until $t = 21$ seconds. Meanwhile, no action is required in the first cavity at $t = 1.5$ seconds; at $t = 20$ seconds, the first cavity 213 is filled with PEN polymer and the pressure increased and held until $t = 21$ seconds (again the hold and cooling stage has been substantially eliminated in the first cavity set by delaying the filling stage until near the end of the hold and cooling stage for the second cavity set). At $t = 21$ seconds, the mold is opened and the preforms 260 are ejected from the second cavities. At $t = 23$ seconds, the shuttle 206 with the still warm neck sleeves is transferred to the second shuttle position as shown in Fig. 6C, and at $t = 24$ seconds the mold is closed as shown in Fig. 6D.

[0041] In this particular embodiment, the first and second core sets 207, 208 are held at a temperature on the order of 60-70°C during both of the first and second molding steps. The first mold cavity (for forming the neck finish sleeve) is on the order of 75-85°C. The PEN polymer has a melt temperature on the order of 275-285°C. The cycle time in the first cavity is on the order of 5-6 seconds; this is the time lapse between the first and second injection steps. The surface

temperature of the sleeve at the time of the second injection is on the order of 100-110°C.

[0042] In the second molding step, the core temperature is on the order of 60-70°C, and the second mold cavity is at a temperature on the order of 5-10°C. The cycle time in the second mold cavity is on the order of 23-25 seconds. The elevated temperature at the outer surface of the sleeve, at the time of the second molding step, causes melt adhesion (including diffusion bonding and chain entanglement) between the PEN polymer of the sleeve and the virgin PET of the outer layer portion 258 which is adjacent the sleeve 250.

Third Preform Embodiment (hot fill)

[0043] A further preform/container embodiment is illustrated in Figs. 8-9. Figs. 8A-8B show a multilayer preform 330 and Figs. 9A-9B show a hot-fill beverage bottle 370 made from the preform of Fig. 8. In this embodiment, a first molded sleeve forms the entire thickness of the neck finish, and is joined at its lower end to a second molded body-forming portion.

[0044] Fig. 8A shows a substantially cylindrical preform 330 (defined by vertical centerline 332) which includes an upper neck portion or finish sleeve 340 bonded to a lower body-forming portion 350. The crystallized neck portion is a monolayer of CPET and includes an upper sealing surface 341 which defines the open top end 342 of the preform, and an exterior surface having threads 343 and a lowermost flange 344. CPET, sold by Eastman Chemical, Kingsport, TN, is a polyethylene terephthalate polymer with nucleating agents which cause the polymer to crystallize during the injection molding process. Below the neck finish 340 is a body-forming portion 350 which includes a flared shoulder-forming section 351, increasing (radially inwardly) in wall thickness from top to bottom, a cylindrical panel-forming section 352 having a substantially uniform wall thickness, and a base-forming section 353. Body-forming section 350 is substantially amorphous and is made of the following three layers in serial order: outer layer 354 of virgin PET; core layer 356 of post-consumer PET; and inner layer 358 of virgin PET. The virgin PET is a low copolymer having 3% comonomers (e.g., cyclohexane dimethanol (CHDM) or isophthalic acid (IPA)) by total weight of the copolymer. A last shot of virgin PET (to clean the nozzle) forms a core layer 359 in the base.

[0045] This particular preform is designed for making a hot-fill beverage container. In this embodiment, the preform has a height of about 96.3mm, and an outer diameter in the panel-forming section 352 of about 26.7mm. The total wall thickness at the panel-forming section 352 is about 4mm, and the thicknesses of the various layers are: outer layer 354 of about 1mm, core layer 356 of about 2mm, and inner layer 358 of about 1mm. The panel-forming section 352 may be stretched at an average planar stretch ratio of about 10:1, as described hereinafter. The planar stretch ratio is the ratio of the average thickness of the preform panel-forming portion 352 to the average thickness of the container panel 383, wherein the "average" is taken along the length of the respective preform or container portion. For hot-fill beverage bottles of about 0.5 to 2.0 liters in volume and about 0.35 to 0.60 millimeters in panel wall thickness, a preferred planar stretch ratio is about 9 to 12, and more preferably about 10 to 11. The hoop stretch is preferably about 3.3 to 3.8 and the axial stretch about 2.8 to 3.2. This produces a container panel with the desired abuse resistance, and a preform sidewall with the desired visual transparency. The specific panel thickness and stretch ratio selected depend on the dimensions of the bottle, the internal pressure, and the processing characteristics (as determined for example, by the intrinsic viscosity of the particular materials employed).

[0046] In order to enhance the crystallinity of the neck portion, a high injection mold temperature is used at the first molding station. In this embodiment, CPET resin at a melt temperature of about 280 to 290°C is injection molded at a mold cavity temperature of about 110 to 120°C and a core temperature of about 5 to 15°C, and a cycle time of about 6 to 7 seconds. The first core set, carrying the still warm neck portions (outer surface temperature of about 115 to 125°C), are then transferred to the second station where multiple second polymers are injected to form the multilayer body-forming portions and melt adhesion occurs between the neck and body-forming portions. The core and/or cavity set at the second station are cooled (e.g., 5 to 15°C core/cavity temperature) in order to solidify the preforms and enable removal from the molds (cycle time of about 23 to 25 seconds) with acceptable levels of post-mold shrinkage. The cores and cavities at both the first and second stations include water cooling/heating passages for adjusting the temperature as desired.

[0047] As used herein, "melt adhesion" between the inner sleeve and outer layer is meant to include various types of bonding which occur due to the enhanced temperature (at the outer surface of the inner sleeve) and pressure (e.g., typical injection molding on the order of 55×10^6 - 103×10^6 N/m² (8000-15,000 psi) during the second molding step, which may include diffusion, chemical, chain entanglement, hydrogen bonding, etc. Generally, diffusion and/or chain entanglement will be present to form a bond which prevents delamination of the layers in the preform, and in the container when filled with water at room temperature (25°C) and dropped from a height of 457mm (eighteen inches) onto a thick steel plate.

[0048] Fig. 8B is an expanded view of the neck finish 340 of preform 330. The monolayer CPET neck finish is formed with a projection 345 at its lower end, which is later surrounded (interlocked) by the virgin PET melt from the inner and outer layers 354, 358 at the second molding station. The CPET neck finish and outermost virgin PET layers of the body

are melt adhered together in this intermediate region (between the lower end of the neck finish sleeve and the upper end of the body-forming region).

[0049] Fig. 9A shows a unitary expanded plastic preform container 370, made from the preform of Fig. 8. The container is about 182.0mm in height and about 71.4mm in (widest) diameter. This 454 cm³ (16-oz.) container is intended for use as a hot-fill non-carbonated juice container. The container has an open top end with the same crystallized neck finish 340 as the preform, with external screw threads 343 for receiving a screw-on cap (not shown). Below the neck finish 340 is a substantially amorphous and transparent expanded body portion 380. The body includes a substantially vertically-disposed sidewall 381 (defined by vertical centerline 372 of the bottle) and base 386. The sidewall includes an upper flared shoulder portion 382 increasing in diameter to a substantially cylindrical panel portion 383. The panel 383 has a plurality of vertically elongated, symmetrically-disposed vacuum panels 385. The vacuum panels move inwardly to alleviate the vacuum formed during product cooling in the sealed container, and thus prevent permanent, uncontrolled deformation of the container. The base 386 is a champagne-style base having a recessed central gate portion 387 and moving radially outwardly toward the sidewall, an outwardly concave dome 388, an inwardly concave chime 389, and a radially increasing and arcuate outer base portion 390 for a smooth transition to the sidewall 381.

[0050] Fig. 9B shows in cross section the multilayer panel portion 383 including an outer layer 392, a core layer 394, and an inner layer 396, corresponding to the outer 354, core 356 and inner 358 layers of the preform. The inner and outer container layers 392, 396 (of virgin PET copolymer) are each about 0.1mm thick, and the core layer 394 (of post-consumer PET) is about 0.2mm thick. The shoulder 382 and base 386 are stretched less and therefore are relatively thicker and less oriented than the panel 383.

Fourth Preform Embodiment

[0051] A fourth preform embodiment is illustrated in Fig. 10. A multilayer preform 130 is made from the method and apparatus of Figs. 1-2, and is adapted to be reheated stretch blow-molded into a refillable carbonated beverage bottle similar to that shown in Fig. 4, but having a thickened base area including the chime for increased resistance to caustic and pressure induced stress cracking.

[0052] In Fig. 10 there is shown a preform 130 which includes a PEN inner sleeve layer 120, and a three-layer outer layer comprising outermost (exterior) virgin PET layer 123, first intermediate (interior) PC-PET layer 124, and second intermediate (interior) virgin PET layer 125. The inner sleeve layer 120 is continuous, having a body portion 121 extending the full length of the preform and throughout the base. The sleeve layer further includes an upper flange 122 which forms the top sealing surface of the preform. The outer layer similarly extends the full length and throughout the bottom of the preform.

[0053] The preform 130 includes an upper neck finish 132, a flared shoulder-forming section 134 which increases in thickness from top to bottom, a panel-forming section 136 having a uniform wall thickness, and a thickened base-forming section 138. Base section 138 includes an upper cylindrical thickened portion 133 (of greater thickness than the panel section 136) which forms a thickened chime in the container base, and a tapering lower portion 135 of reduced thickness for forming a recessed dome in the container base. A last shot of virgin PET (to clean the nozzle) forms a core layer 139 in the base. A preform having a preferred cross-section for refill applications is described in U.S. Patent 5,066,528 granted November 19, 1991 to Krishnakumar et al., which is hereby incorporated by reference in its entirety.

[0054] This particular preform is designed for making a refillable carbonated beverage container. The use of an inner sleeve 120 of a PEN homopolymer, copolymer, or blend provides reduced flavor absorption and increased thermal stability for increasing the wash temperature. The inner PEN sleeve can be made relatively thin according to the method of Fig. 1. The interior PC-PET layer 124 can be made relatively thick to reduce the cost of the container, without significantly affecting performance. In this example, the preform has a height of about 7.130 inches (181.1 mm), and an outer diameter in the panel-forming section 136 of about 1.260 inches (32.0mm). At the panel-forming section 136, the total wall thickness is about 0.230 inches (5.84 mm), and the thicknesses of the various layers are: inner layer 120 of about 0.040 inches (1.0 mm), outermost layer 123 of about 0.040 inches (1.0 mm), first intermediate layer 124 of about 0.130 inches (3.30 mm), and second intermediate layer 125 of about 0.020 inches (0.5 mm). The panel-forming section 136 may be stretched at an average planar stretch ratio of about 10.5:1, as described hereinafter. The planar stretch ratio is the ratio of the average thickness of the preform panel-forming portion 136 to the average thickness of the container panel (see for example sidewall 46 in Fig. 4), wherein the "average" is taken along the length of the respective preform or container portion. For refillable carbonated beverage bottles of about 0.5 to 2.0 liters in volume and about 0.5 to 0.8 millimeters in panel wall thickness, a preferred planar stretch ratio is about 7.5-10.5, and more preferably about 9.0-10.5. The hoop stretch is preferably about 3.2-3.5 and the axial stretch about 2.3-2.9. This produces a container panel with the desired abuse resistance, and a preform sidewall with the desired visual transparency. The specific panel thickness and stretch ratio selected depend on the dimensions of the bottle, the internal pressure (e.g., 2 atmospheres for beer and 4 atmospheres for soft drinks), and the processing characteristics (as determined for example, by the intrinsic viscosity of the particular materials employed).

[0055] In order to provide a thin PEN sleeve layer (e.g. 0.5 to 1.0 mm), a suitable mold cavity temperature would be on the order of 100 to 110°C and core temperature of about 5 to 15°C, for a PET melt temperature of about 285 to 295°C and cycle time of about 6 to 7 seconds. The first core set and warm inner layer are then immediately transferred to the second station where the outer layers are injected and bonding occurs between the inner and outer layers (e.g., exterior surface of inner PEN sleeve layer at about 90 to 100°C and innermost PET layer at about 260 to 275°C). The first core set and/or second cavity set at the second station are cooled (e.g., about 5 to 15°C) in order to solidify the perform and enable removal from the mold. The cores and cavities at both the first and second stations include water cooling/heating passages for adjusting the temperature as desired.

[0056] In this embodiment, the inner sleeve layer 120 is made from a high-PEN copolymer having 90% PEN/10% PET by total weight of the layer, and in the container panel is about 0.004 inches (0.10 mm) thick. The outermost layer 123 is a virgin PET low copolymer having 3% comonomers (e.g., CHDM or IPA), and in the container panel is about 0.004 in (0.10 mm) thick. The first intermediate layer 124 is PC-PET, and in the container panel is about 0.012 in (0.30 mm) thick. The second intermediate layer 125 is the same virgin PET low copolymer as outermost layer 123, and in the container panel is about 0.002 in (0.05 mm) thick. The container shoulder and base (see 44 and 48 in Fig. 4A) are stretched less and therefore are thicker and less oriented than the panel (see 46 in Fig. 4A).

Fifth Preform Embodiment

[0057] Fig. 11 illustrates another preform embodiment for making a refillable carbonated beverage container. This preform has an additional outermost layer in the base only for increasing caustic stress crack resistance, while maximizing the use of post-consumer PET for reducing the cost. The preform 160 includes an upper neck finish 162, shoulder-forming portion 164, panel-forming section 166, and base-forming portion 168. The inner layer 170 has a body portion 171 which is continuous throughout the length (including the bottom) of the preform and includes an upper flange 172 forming the top sealing surface. The inner layer is virgin PET. An outer layer 173 of PC-PET extends throughout the length of the preform, and forms a single outer layer in the neck finish and panel-forming section. In the base-forming portion an additional exterior layer 174 of high IV virgin PET is provided to enhance the caustic stress crack resistance of the blown container. A thin interior layer 175 of the high IV virgin PET may also be formed according to the sequential injection process previously referenced. A last shot 176 of high IV virgin PET is used to clear out the PC-PET from the nozzle section. The outer base layer 174 is preferably a high IV virgin PET (homopolymer or copolymer) having an intrinsic viscosity of at least about 0.76, and preferably in the range of 0.76 to 0.84. The resulting container may be either a footed or champagne base container.

Sixth Preform Embodiment

[0058] Fig. 12 shows another preform embodiment including a high-temperature neck finish sleeve 190 and a single outer layer 194 for forming a hot-fill container. The preform 180 includes a neck finish 182, shoulder-forming portion 184, panel-forming portion 186, and base-forming portion 188. The inner sleeve 190 includes a neck finish portion 191, extending substantially along the length of the upper threaded neck finish portion 182 of the container, and an upper flange 192 forming a top sealing surface. The inner sleeve is formed of a thermal resistant (high T_g) material such as a PEN homopolymer, copolymer or blend. Alternatively, the sleeve may be formed of CPET, sold by Eastman Chemical, Kingsport, TN, a polyethylene terephthalate polymer with nucleating agents which cause the polymer to crystallize during the injection molding process.

[0059] The outer layer 194 is made of virgin PET. This preform is intended for making hot-fill containers, wherein the inner sleeve 190 provides additional thermal stability at the neck finish.

[0060] In further alternative embodiments, a triple outer layer of virgin PET, PC-PET, and virgin PET may be used.

Alternative Constructions and Materials

[0061] There are numerous preform and container constructions, and many different injection moldable materials, which may be adapted for a particular food product and/or package, filling, and manufacturing process. Additional representative examples are given below.

[0062] Thermoplastic polymers useful in the present invention include polyesters, polyamides and polycarbonates. Suitable polyesters include homopolymers, copolymers or blends of polyethylene terephthalate (PET), polybutylene terephthalate (PBT), polypropylene terephthalate (PPT), polyethylene naphthalate (PEN), and a cyclohexane dimethanol/PET copolymer, known as PETG (available from Eastman Chemical, Kingsport, TN). Suitable polyamides (PA) include PA6, PA6,6, PA6,4, PA6,10, PA11, PA12, etc. Other useful thermoplastic polymers include acrylic/imide, amorphous nylon, polyacrylonitrile (PAN), polystyrene, crystallizable nylon (MXD-6), polyethylene (PE), polypropylene (PP), and polyvinyl chloride (PVC).

[0063] Polyesters based on terephthalic or isophthalic acid are commercially available and convenient. The hydroxy compounds are typically ethylene glycol and 1,4-di-(hydroxy methyl)-cyclohexane. The intrinsic viscosity for phthalate polyesters are typically in the range of 0.6 to 1.2, and more particularly 0.7 to 1.0 (for O-chlorophenol solvent). 0.6 corresponds approximately to a viscosity average molecular weight of 59,000, and 1.2 to a viscosity average molecular weight of 112,000. In general, the phthalate polyester may include polymer linkages, side chains, and end groups not related to the formal precursors of a simple phthalate polyester previously specified. Conveniently, at least 90 mole percent will be terephthalic acid and at least 90 mole percent an aliphatic glycol or glycols, especially ethylene glycol.

[0064] Post-consumer PET (PC-PET) is a type of recycled PET prepared from PET plastic containers and other recyclables that are returned by consumers for a recycling operation, and has now been approved by the FDA for use in certain food containers. PC-PET is known to have a certain level of I.V. (Intrinsic viscosity), moisture content, and contaminants. For example, typical PC-PET (having a flake size of one-half inch maximum), has an I.V. average of about 0.66 dl/g, a relative humidity of less than 0.25%, and the following levels of contaminants:

PVC: < 100 ppm
 aluminum: < 50 ppm
 olefin polymers (HDPE, LDPE, PP): < 500 ppm
 paper and labels: < 250 ppm
 colored PET: < 2000 ppm
 other contaminants: < 500 ppm

PC-PET may be used alone or in one or more layers for reducing the cost or for other benefits.

[0065] Also useful as a base polymer or as a thermal resistant and/or high-oxygen barrier layer is a packaging material with physical properties similar to PET, namely polyethylene naphthalate (PEN). PEN provides a 3-5X improvement in barrier property and enhanced thermal resistance, at some additional expense. Polyethylene naphthalate (PEN) is a polyester produced when dimethyl 2,6-naphthalene dicarboxylate (NDC) is reacted with ethylene glycol. The PEN polymer comprises repeating units of ethylene 2,6 naphthalate. PEN resin is available having an inherent viscosity of 0.67 dl/g and a molecular weight of about 20,000 from Amoco Chemical Company, Chicago, Illinois. PEN has a glass transition temperature T_g of about 123°C, and a melting temperature T_m of about 267°C.

[0066] Oxygen barrier layers include ethylene/vinyl alcohol (EVOH), PEN, polyvinyl alcohol (PVOH), polyvinylidene chloride (PVDC), nylon 6, crystallizable nylon (MXD-6), LCP (liquid crystal polymer), amorphous nylon, polyacrylonitrile (PAN) and styrene acrylonitrile (SAN).

[0067] The intrinsic viscosity (I.V.) effects the processability of the resins. Polyethylene terephthalate having an intrinsic viscosity of about 0.8 is widely used in the carbonated soft drink (CSD) industry. Polyester resins for various applications may range from about 0.55 to about 1.04, and more particularly from about 0.65 to 0.85 dl/g. Intrinsic viscosity measurements of polyester resins are made according to the procedure of ASTM D-2857, by employing 0.0050 ± 0.0002 g/ml of the polymer in a solvent comprising o-chlorophenol (melting point 0°C), respectively, at 30°C. Intrinsic viscosity (I.V.) is given by the following formula:

$$I.V. = (\ln(V_{Soln.}/V_{Sol.}))/C$$

where:

$V_{Soln.}$ is the viscosity of the solution in any units;
 $V_{Sol.}$ is the viscosity of the solvent in the same units; and
 C is the concentration in grams of polymer per 100 mls of solution.

[0068] The blown container body should be substantially transparent. One measure of transparency is the percent haze for transmitted light through the wall (H_T) which is given by the following formula:

$$H_T = [Y_d + (Y_d + Y_s)] \times 100$$

where Y_d is the diffuse light transmitted by the specimen, and Y_s is the specular light transmitted by the specimen. The diffuse and specular light transmission values are measured in accordance with ASTM Method D 1003, using any standard color difference meter such as model D25D3P manufactured by Hunterlab, Inc. The container body should have a percent haze (through the panel wall) of less than about 10%, and more preferably less than about 5%.

[0069] The preform body-forming portion should also be substantially amorphous and transparent, having a percent

haze across the wall of no more than about 10%, and more preferably no more than about 5%.

[0070] The container will have varying levels of crystallinity at various positions along the height of the bottle from the neck finish to the base. The percent crystallinity may be determined according to ASTM 1505 as follows:

$$\% \text{ crystallinity} = [(ds - da)/(dc - da)] \times 100$$

where ds = sample density in g/cm³, da = density of an amorphous film of zero percent crystallinity, and dc = density of the crystal calculated from unit cell parameters. The panel portion of the container is stretched the greatest and preferably has an average percent crystallinity in at least the outer layer of at least about 15%, and more preferably at least about 20%. For primarily PET polymers, a 15-25% crystallinity range is useful in refill and hot-fill applications.

[0071] Further increases in crystallinity can be achieved by heat setting to provide a combination of strain-induced and thermal-induced crystallization. Thermal-induced crystallinity is achieved at low temperatures to preserve transparency, e.g., holding the container in contact with a low temperature blow mold. In some applications, a high level of crystallinity at the surface of the sidewall alone is sufficient.

[0072] As a further alternative embodiment, the preform may include one or more layers of an oxygen scavenging material. Suitable oxygen scavenging materials are described in U.S. Serial No. 08/355,703 filed December 14, 1994 by Collette et al., entitled "Oxygen Scavenging Composition For Multilayer Preform And Container," which is hereby incorporated by reference in its entirety. As disclosed therein, the oxygen scavenger may be a metal-catalyzed oxidizable organic polymer, such as a polyamide, or an anti-oxidant such as phosphite or phenolic. The oxygen scavenger may be mixed with PC-PET to accelerate activation of the scavenger. The oxygen scavenger may be advantageously combined with other thermoplastic polymers to provide the desired injection molding and stretch blow molding characteristics for making substantially amorphous injection molded preforms and substantially transparent biaxially oriented polyester containers. The oxygen scavenger may be provided as an interior layer to retard migration of the oxygen scavenger or its byproducts, and to prevent premature activation of the scavenger.

[0073] Refillable containers must fulfill several key performance criteria in order to achieve commercial viability, including:

1. high clarity (transparency) to permit visual on-line inspection;
2. dimensional stability over the life of the container; and
3. resistance to caustic wash induced stress cracking and leakage.

Generally, a refillable plastic bottle must maintain its functional and aesthetic characteristics over a minimum of 10 and preferably 20 cycles or loops to be economically feasible. A cycle is generally comprised of (1) an empty hot caustic wash, (2) contaminant inspection (before and/or after wash) and product filling/capping, (3) warehouse storage, (4) distribution to wholesale and retail locations and (5) purchase, use and empty storage by the consumer, followed by eventual return to the bottler.

[0074] A test procedure for simulating such a cycle would be as follows. As used in this specification and claims, the ability to withstand a designated number of refill cycles without crack failure and/or with a maximum volume change is determined according to the following test procedure.

[0075] Each container is subjected to a typical commercial caustic wash solution prepared with 3.5% sodium hydroxide by weight and tap water. The wash solution is maintained at a designated wash temperature, e.g., 60°C. The bottles are submerged uncapped in the wash for 15 minutes to simulate the time/temperature conditions of a commercial bottle wash system. After removal from the wash solution, the bottles are rinsed in tap water and then filled with a carbonated water solution at 4.0 ± 0.2 atmospheres (to simulate the pressure in a carbonated soft drink container), capped and placed in a 38°C convection oven at 50% relative humidity for 24 hours. This elevated oven temperature is selected to simulate longer commercial storage periods at lower ambient temperatures. Upon removal from the oven, the containers are emptied and again subjected to the same refill cycle, until failure.

[0076] A failure is defined as any crack propagating through the bottle wall which results in leakage and pressure loss. Volume change is determined by comparing the volume of liquid the container will hold at room temperature, both before and after each refill cycle.

[0077] A refillable container can preferably withstand at least 20 refill cycles at a wash temperature of 60°C without failure, and with no more than 1.5% volume change after 20 cycles.

[0078] In this invention, a higher level of crystallization can be achieved in the neck finish compared to prior art processes which crystallize outside the mold. Thus, the preform neck finish may have a level of crystallinity of at least about 30%. As a further example, a neck finish made of a PET homopolymer can be molded with an average percent crystallinity of at least about 35%, and more preferably at least about 40%. To facilitate bonding between the neck portion and body-forming portion of the preform, one may use a thread split cavity, wherein the thread section of the

mold is at a temperature above 60°C, and preferably above 75°C.

[0079] As an additional benefit, a colored neck finish can be produced, while maintaining a transparent container body.

[0080] The neck portion can be monolayer or multilayer and made of various polymers other than CPET, such as arylate polymers, polyethylene naphthalate (PEN), polycarbonates, polypropylene, polyimides, polysulfones, acrylonitrile styrene, etc. As a further alternative, the neck portion can be made of a regular bottle-grade homopolymer or low copolymer PET (i.e., having a low crystallization rate), but the temperature or other conditions of the first molding station can be adjusted to crystallize the neck portion.

[0081] Other benefits include the achievement of higher hot-fill temperatures (i.e., above 85°C) because of the increased thermal resistance of the finish, and higher refill wash temperatures (i.e., above 60°C). The increased thermal resistance is also particularly useful in pasteurizable containers.

[0082] Figs. 13A-13B illustrate graphically the change in melt temperature and orientation temperature for PET/PEN compositions, as the weight percent of PEN increases from 0 to 100. There are three classes of PET/PEN copolymers or blends: (a) a high-PEN concentration having on the order of 80-100% PEN and 0-20% PET by total weight of the copolymer or blend, which is a strain-hardenable (orientable) and crystallizable material; (b) a mid-PEN concentration having on the order of 20-80% PEN and 80-20% PET, which is an amorphous non-crystallizable material that will not undergo strain hardening; and (c) a low-PEN concentration having on the order of 1-20% PEN and 80-99% PET, which is a crystallizable and strain-hardenable material. A particular PEN/PET polymer or blend can be selected from Figs. 13A-13B based on the particular application.

[0083] Fig. 14 illustrates a particular embodiment of a combined infrared (IR) and radio frequency (RF) heating system for reheating previously molded and cooled preforms (i.e., for use in a two-stage reheat injection mold and stretch blow process). This system is intended for reheating preforms having layers with substantially different orientation temperatures. For example, in the fourth preform embodiment the high-PEN inner layer 120 has an orientation temperature much higher than the virgin PET low copolymer and PC-PET outer layers 123-125. PEN homopolymer has a minimum orientation temperature on the order of 260°F (127°C), based on a glass transition temperature on the order of 255°F (123°C). PEN homopolymer has a preferred orientation range of about 270-295°F (132-146°C). In contrast, PET homopolymer has a glass transition temperature on the order of 175°F (80°C). At the minimum orientation temperature of PEN homopolymer, PET homopolymer would begin to crystallize and would no longer undergo strain hardening (orientation), and the resulting container would be opaque and have insufficient strength.

[0084] Returning to Fig. 14, this combined reheating apparatus may be used with preforms having a substantial disparity in orientation temperatures between layers. The preforms 130 are held at the upper neck finish by a collet 107 and travel along an endless chain 115 through stations A, B and C in serial order. Station A is a radiant heating oven in which the preforms are rotated while passing by a series of quartz heaters. The heating of each preform is primarily from the exterior surface and heat is transmitted across the wall to the inner layer. The resulting heat or temperature profile is higher at the exterior surface of the preform than at the interior surface. The time and temperature may be adjusted in an attempt to equilibrate the temperature across the wall.

[0085] In this embodiment, it is desired to heat the inner PEN layer at a higher temperature because of PEN's higher orientation temperature. Thus, the preforms (across the wall) are brought up to an initial temperature of about 160°F (71°C) at station A, and are then transferred to station B which utilizes microwave or radio frequency heaters. These highfrequency dielectric heaters provide a reverse temperature profile from that of the quartz heaters, with the interior surface of the preform being heated to a higher temperature than that of the exterior surface. Fig. 14 shows the preforms 130 traveling between electrode plates 108 and 109, which are connected to RF generator 110 and ground respectively. At station B, the inner layer is brought up to a temperature of about 295°F (146°C), and the outer layer to a temperature of about 200°F (93°C). Finally, the preforms are passed to station C, which is similar to station A. At station C the quartz heaters bring the preforms to a temperature of about 280°F (138°C) at the inner layer and about 210°F (99°C) at the outer layer. The reheated preforms are then sent to a blow mold for stretch blow molding. A more detailed description of hybrid reheating of polyester preforms including a combination of quartz oven reheating and radio frequency reheating is described in U.S. Patent 4,731,513 to Collette entitled "Method Of Reheating Preforms For Forming Blow Molded Hot Fillable Containers," which issued March 15, 1988, and is hereby incorporated by reference. In addition, additives may be provided in either or both of the PET and PEN layers to make them more receptive to radio frequency heating.

[0086] In a preferred thin sleeve/thick outer layer embodiment, the thin inner layer sleeve may have a thickness on the order of 0.02 to 0.06 inch (0.5 to 1.5mm), while the thick outer layer has a wall thickness on the order of 0.10 to 0.25 inch (2.50 to 6.35mm). The inner layer may comprise on the order of 10-20% by total weight of the preform. This represents an improvement over the prior art single injection cavity process for making multilayer preforms. Also, the weight of one or more outer layers (such as a layer of PC-PET) can be maximized.

[0087] While there have been shown and described several embodiments of the present invention, it will be obvious to those skilled in the art that various changes and modifications may be made therein without departing from the scope

of the invention as defined by the appending claims.

Claims

- 5 1. Method of reducing the inner layer thickness and improving the layer adhesion in a multilayer injection-molded plastic article, the method comprising:
 10 firstly molding an inner sleeve layer (20) between a first mold cavity (11) and core (9), the first mold cavity being heated to maintain an outer surface of the inner sleeve layer at an elevated temperature;
 transferring the core (9) and sleeve layer (20) to a second mold cavity (12) and secondly molding an outer
 layer (22) over the sleeve layer while the outer surface is at the elevated temperature, the outer layer (22)
 having a thickness greater than the thickness of the inner sleeve layer (20), where the elevated temperature
 15 is selected to provide melt adhesion between the inner sleeve (20) and the outer layer (22) during the second molding step.
2. The method of claim 1, wherein the melt adhesion between the inner sleeve (20) and outer layer (22) includes diffusion bonding.
- 20 3. The method of claim 1, wherein the melt adhesion between the inner sleeve (20) and outer layer (22) includes chain entanglement.
4. The method of claim 1, wherein the sleeve forms an upper sleeve portion (250, 340, 190) of the article, and the outer layer forms a lower body portion (260, 350, 180) of the article.
- 25 5. The method of claim 4, wherein a lower end of the upper sleeve portion and an upper end of the lower body portion are joined in an intermediate portion of the article.
6. The method of claim 1, wherein the first molding step forms the inner sleeve (120, 170) as a full-length inner layer (121, 171) and upper surface (122, 172) of the article.
- 30 7. The method of claim 1, wherein the first molding step forms the inner sleeve (250) as an upper length portion of the article and an upper surface of the article.
8. The method of claim 1, wherein the outer layer (260, 350) comprises multiple outer layers.
- 35 9. The method of claim 1, wherein the article is a preform (30, 330, 130, 160, 180).
10. The method of claim 9, wherein the first molding step forms a neck finish portion (250, 340, 190) of the preform.
- 40 11. The method of claim 10, wherein the neck finish portion is molded from a polymer which crystallizes during the first molding step.
12. The method of claim 10, wherein the neck finish portion is molded from a first polymer material having a higher glass transition temperature than a second polymer material which forms the outer layer.
- 45 13. The method of claim 1, wherein the sleeve has a weight in a range on the order of 10 to 20 percent of a total weight of the article.
14. The method of claim 1, wherein the sleeve has a wall thickness in a range on the order of 0.5 to 1.5mm (0.02 to 0.06 inch).
- 50 15. The method of claim 14, wherein the outer layer has a wall thickness in a range on the order of 2.50 to 6.35mm (0.10 to 0.25 inch).
- 55 16. The method of claim 1, wherein the inner sleeve is formed of a first material having a first melt temperature, and the outer layer includes a second layer adjacent the inner sleeve and made of a second material having a second melt temperature lower than the first melt temperature.

17. The method of claim 1, wherein the first mold cavity (11) is at a first cavity temperature and the second mold cavity (12) is at a second cavity temperature lower than the first cavity temperature.
18. The method of claim 17, wherein the core (9) is at a core temperature which is less than the first cavity temperature.
19. The method of claim 1, wherein the inner sleeve is formed of a first material having a first T_g , and the elevated temperature is in a range on the order of 5-20°C below the first T_g .
20. The method of claim 1, wherein the sleeve is molded from a first material selected from the group consisting of homopolymers, copolymers, and blends of polyethylene naphthalate (PEN).
21. The method of any one of claims 1 and 20, wherein the outer layer includes at least one layer molded from a second material selected from the group consisting of polyethylene terephthalate (PET), an oxygen scavenging material, recycled PET, polyethylene, polypropylene, polyacrylate, polycarbonate, polyacrylonitrile, nylon, and copolymers and blends thereof.
22. The method of claim 1, wherein the article has a sidewall portion in which the inner sleeve has a first thickness (t_1) and the outer layer has a second thickness (t_2), and the ratio of $t_2:t_1$ is greater than on the order of 4:1.
23. The method of claim 1, wherein the article has a first thickness (t_1) and the outer layer has a second thickness (t_2), and the ratio of $t_2:t_1$ is on the order of from 1.2:1 to 8:1.
24. The method of claim 1, wherein the inner sleeve (340) is substantially crystallized and the outer layer (350) is substantially amorphous.
25. The method of claim 1, wherein the inner sleeve is made of a first material and the outer layer is made of a second material, and the second material has a lower crystallization rate compared to the first material.
26. The method of claim 1, wherein first and second cores (9, 10) are provided, and wherein during a first cycle the first core (9) is positioned in the first mold cavity (11) to form a first inner sleeve, and the second core (10), having a second inner sleeve positioned thereon, is simultaneously positioned in the second mold cavity (12) for molding a second outer layer on the second inner sleeve.
27. The method of claim 26, wherein the first molding step includes an initial no-action period while the second molding step proceeds in order to facilitate the transfer while the outer surface of the sleeve layer is at the elevated temperature.
28. The method of claim 1, wherein the sleeve is molded of a first material selected from the group consisting of polyester, polyester with nucleating agents, acrylate, polyethylene naphthalate (PEN), polycarbonate, polypropylene, polyamide, polysulfone, acrylonitrile styrene, and copolymers and blends thereof.
29. The method of claim 28, wherein the outer layer includes a second material selected from the group consisting of homopolymers, copolymers, and blends of any one or more of: polyethylene terephthalate (PET), polyethylene naphthalate (PEN), and recycled PET.
30. The method of claim 1, wherein the article (330) has a body portion (350) and the method further comprises expanding the body portion of the article to form an expanded article (370) having a substantially transparent and biaxially-oriented body portion (380).
31. The method of claim 1, wherein the method further comprises cooling the article (330) below a first glass transition temperature of a first material in the article, reheating the article above the first glass transition temperature, and expanding the reheated article to form an expanded article (370).
32. The method of claim 31, wherein the expanded article (370) has a high T_g or crystallized upper neck finish portion (340) and a substantially transparent, biaxially-oriented body portion (380).
33. An apparatus for making multi-layer injection-molded plastic articles comprising:

a first mold cavity set (11) and a second mold cavity set (12), each first cavity being adapted to form an inner sleeve layer (20) and each second cavity being adapted to form an outer layer (22), the outer layer (22) having a thickness greater than the thickness of the inner sleeve layer (20);
 5 a transfer mechanism (2) with first and second core sets (9, 10) for successively positioning the first and second core sets in the first and second cavity sets;
 wherein the first core set (9) is positionable in the first cavity set (11) for molding a set of inner sleeve layers (20) on the first core set, while the second core set (10) is positionable in the second cavity set (12) for molding, over a previously-molded set of inner sleeve layers on the second core set, a second set of outer layers (22);
 10 and
 means for heating (15) the first cavity set so as to maintain an outer surface of the inner sleeve layer (20) at an elevated temperature during transfer and molding of the outer layer (22) thereover, the elevated temperature being selected to provide melt adhesion between the inner sleeve and outer layer.

34. The apparatus of claim 33, wherein the first cavity (11) and core (9) define a first wall thickness (t_1) and the second cavity (12) and core (10) define a second wall thickness (t_2), and wherein a ratio of $t_2:t_1$ is greater than on the order of 4:1.

35. The apparatus of claim 33, wherein the transfer mechanism is a rotatable turret (2).

20 36. The apparatus of claim 33, wherein the transfer mechanism is a reciprocating shuttle (206).

37. The apparatus of claim 33, including means for initiating molding of the outer layers in the second cavity set while maintaining a no-action period in the first cavity set in order to facilitate transfer while the outer surface of the sleeve layer is at the elevated temperature.

25 38. The method of claim 1 comprising:

injection molding a first thermoplastic material to form a first preform portion (340) including the inner sleeve layer (20) having an average percent crystallinity of at least about 30%; and
 30 injection molding a second thermoplastic material to form a second preform portion (350) including the outer sleeve (22) which remains substantially amorphous.

39. The method of claim 38, wherein the first portion is substantially a neck portion (340) and the second portion is substantially a body-forming portion (350).

35 40. The method of claim 38, wherein the second material has a lower crystallization rate compared to the first material.

41. The method of claim 40, wherein the first material is selected from the group consisting of polyester, polyester with nucleating agents, arylate polymers, polyethylene naphthalate (PEN), polycarbonate, polypropylene, polyamide, polysulfone, acrylonitrile styrene, and copolymers and blends thereof.

42. The method of claim 41, wherein the second material is selected from the group consisting of homopolymers, copolymers and blends of any one or more of: polyethylene terephthalate (PET), polyethylene naphthalate (PEN), and recycled PET.

45 43. The method of claim 41, further comprising expanding the second portion (350) to form a substantially transparent and biaxially-oriented body (380) of a container (370).

50 44. The method of claim 1, comprising:

first molding the inner sleeve (20) on a core (9) positioned in the first mold cavity (11), the first molding step including a filling stage and a pressure boost stage but substantially no holding and cooling stage so as to maintain the outer surface of the inner sleeve at an elevated temperature for a second molding step;
 55 removing the sleeve (20) on the core (9) and transferring the same without substantial delay to the second mold cavity (12); and
 second molding the outer layer (22) over the sleeve (20) in the second mold cavity (12) to form the multi-layer injection-molded article.

45. The method of claim 1, wherein the inner sleeve is made of a PEN polymer material and the elevated temperature is in range on the order of 60-120°C.
46. The method of claim 45, wherein the first molding step has a cycle time on the order of no greater than 8 seconds.
47. The method of claim 45, wherein the cycle time is in a range on the order of 4-8 seconds.
48. The method of claim 45, wherein the first cavity temperature is in a range on the order of 40-120°C and the core temperature is in a range on the order of 5-80°C.
49. The method of claim 48, wherein the first cavity temperature is in a range on the order of 75-95 °C and the core temperature is in a range on the order of 60-70°C.
50. The method of claim 48, wherein the first cavity temperature is in a range on the order of 100-110°C and the core temperature is in a range on the order of 5-15°C.
51. The method of claim 48, wherein the PEN polymer material has a melt temperature in a range on the order of 275-295 °C and the elevated temperature is in a range on the order of 90-110°C.
52. The method of claim 1, wherein the outer layer includes a PET polymer material adjacent the inner sleeve, the PET polymer material having a melt temperature in a range on the order of 260-275°C and the second molding step being carried out at a cavity pressure in a range on the order of $55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi).
53. The method of claim 1, wherein the inner sleeve is made of a polyester polymer material which is crystallized during the first molding step and the elevated temperature is in a range on the order of 80-140°C.
54. The method of claim 53, wherein the first molding step has a cycle time on the order of no greater than 8 seconds.
55. The method of claim 54, wherein the cycle time is in a range on the order of 5-8 seconds.
56. The method of claim 53, wherein the first cavity temperature is in a range on the order of 80-150°C and the core temperature is in a range on the order of 5-60°C.
57. The method of claim 56, wherein the first cavity temperature is in a range on the order of 110-120°C and the core temperature is in a range on the order of 5-15°C.
58. The method of claim 53, wherein the polyester polymer material has a melt temperature in a range on the order of 280-290°C and the elevated temperature is in a range on the order of 115-125°C.
59. The method of claim 53, wherein the outer layer includes a PET polymer material adjacent the inner sleeve, the PET polymer material having a melt temperature in a range on the order of 270-285°C and the second molding step being carried out at a cavity pressure in a range on the order of $55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi).
60. The method of claim 44, wherein:
the inner sleeve is made of a PEN polymer material;
during the second molding step the outer surface of the sleeve is at an elevated temperature in a range on the order of 100-110°C and the outer layer includes a first outer layer of a PET polymer material adjacent the inner sleeve, and wherein the PET polymer material has a melt temperature in a range on the order of 260-275°C and the second molding step is carried out at a cavity pressure in a range on the order of $55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi) to achieve melt adhesion between the inner sleeve and the outer layer during the second molding step.
61. The method of claim 44, wherein:
an inner sleeve is made of a PEN polymer material mold;
during the second molding step the outer surface of the sleeve is at an elevated temperature in a range on the order of 90-100°C and the outer layer includes a first outer layer of a PET polymer material adjacent the

inner sleeve, and wherein the PET polymer material has a melt temperature in a range on the order of 260-275°C and the second molding step is carried out at a cavity pressure in the range on the order of $55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi) to achieve melt adhesion between the inner sleeve and the outer layer during the second molding step.

62. The method of claim 44, wherein:

the inner sleeve is made of a polyester polymer material which is crystallized on the core during the first molding step; and
during the second molding step the outer surface of the sleeve is at an elevated temperature in a range on the order of 115-125°C, and the outer layer includes a first outer layer of a PET polymer adjacent the inner sleeve and wherein the PET polymer material has a melt temperature in a range on the order of 270-285°C and the second molding step is carried out at a cavity pressure in the range on the order of $55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi) to achieve melt adhesion between the inner sleeve and the outer layer during the second molding step.

63. The method of any one of claims 44, 60, 61 and 62, wherein the sleeve has a weight in a range on the order of 10 to 20 percent of a total weight of the article.

64. The method of any one of claims 44, 60, 61 and 62, wherein the sleeve has a wall thickness in a range on the order of 0.5 to 1.5mm (0.02 to 0.06 inch).

65. The method of any one of claims 44, 60, 61, 62 and 64, wherein the outer layer has a wall thickness in a range on the order of 2.50 to 6.35mm (0.10 to 0.25 inch).

66. The method of claim 44, wherein the inner sleeve is made of a PEN polymer material and the elevated temperature is in a range on the order of 60-120°C.

67. The method of claim 44, wherein the first molding step has a cycle time on the order of no greater than 8 seconds.

68. The method of claim 44, wherein the cycle time is in a range on the order of 4-8 seconds.

69. The method of claim 44, wherein the first cavity temperature is in a range on the order of 40-120°C and the core temperature is in a range on the order of 5-80°C.

70. The method of claim 69, wherein the first cavity temperature is in a range on the order of 75-95 °C and the core temperature is in a range on the order of 60-70°C.

71. The method of claim 69, wherein the first cavity temperature is in a range on the order of 100- 110°C and the core temperature is in a range on the order of 5-15°C.

72. The method of claim 66, wherein the PEN polymer material has a melt temperature in a range on the order of 275-295°C and the elevated temperature is in a range on the order of 90-110°C.

73. The method of claim 66, wherein the outer layer includes a PET polymer material adjacent the inner sleeve, the PET polymer material having a melt temperature in a range on the order of 260-275 °C and the second molding step being carried out at a cavity pressure in a range on the order of $55 \times 10^6 - 103 \times 10^6 \text{ N/m}^2$ (8000-15,000 psi).

74. The method of claim 44, wherein the inner sleeve is made of a polyester polymer material which is crystallized during the first molding step and the elevated temperature is in a range on the order of 80-140°C.

75. The method of claim 74, wherein the first molding step has a cycle time on the order of no greater than 8 seconds.

76. The method of claim 74, wherein the cycle time is in a range on the order of 5-8 seconds.

77. The method of claim 74, wherein the first cavity temperature is in a range on the order of 80-150°C and the core temperature is in a range on the order of 5-60°C.

78. The method of claim 77, wherein the first cavity temperature is in a range on the order of 110-120°C and the core temperature is in a range on the order of 5-15°C.

79. The method of claim 74, wherein the polyester polymer material has a melt temperature in a range on the order of 280-290°C and the elevated temperature is in a range on the order of 115-125°C.

80. The method of claim 74, wherein the outer layer includes a PET polymer material adjacent the inner sleeve, the PET polymer material having a melt temperature in a range on the order of 270-285°C and the second molding step being carried out at a cavity pressure in a range on the order of 55×10^6 - 103×10^6 N/m² (8000-15,000 psi).

Patentansprüche

1. Verfahren zum Reduzieren der Innenschichtdicke und zum Verbessern der Schichthaftung in einem vielschichtigen spritzgeformten Kunststoffartikel, wobei das Verfahren umfaßt:

erstens Formen einer Innenhülsenschicht (20) zwischen einem ersten Formhohlraum (11) und einem Kern (9), wobei der erste Formhohlraum erhitzt wird, damit eine Außenfläche der Innenhülsenschicht auf einer angehobenen Temperatur gehalten wird;
Übergeben des Kernes (9) und der Hülsenschicht (20) an einen zweiten Formhohlraum (12) und zweitens Formen einer Außenschicht (22) über der Hülsenschicht, während die Außenfläche die angehobene Temperatur hat, wobei die Außenschicht (22) eine Dicke hat, die größer ist als die Dicke der Innenhülsenschicht (20), wobei die angehobene Temperatur so ausgewählt ist, daß eine Schmelzhaftung zwischen der Innenhülse (20) und der Außenschicht (22) während des zweiten Formungsschrittes erreicht wird.

2. Verfahren nach Anspruch 1, wobei die Schmelzhaftung zwischen der Innenhülse (20) und der Außenschicht (22) eine Diffusions-Kontaktherstellung beinhaltet.

3. Verfahren nach Anspruch 1, wobei die Schmelzhaftung zwischen der Innenhülse (20) und der Außenschicht (22) eine Kettenverknüpfung umfaßt.

4. Verfahren nach Anspruch 1, wobei die Hülse einen oberen Hülsenabschnitt (250, 340, 190) des Artikels bildet und die Außenschicht einen unteren Körperabschnitt (260, 350, 180) des Artikels.

5. Verfahren nach Anspruch 4, wobei ein unteres Ende des oberen Hülsenabschnittes und ein oberes Ende des unteren Körperabschnittes in einem Zwischenabschnitt des Artikels miteinander verbunden sind.

6. Verfahren nach Anspruch 1, wobei der erste Formungsschritt die Innenhülse (120, 170) als eine Innenschicht (121, 171) mit voller Länge und obere Oberfläche (122, 172) des Artikels formt.

7. Verfahren nach Anspruch 1, wobei der erste Formungsschritt die Innenhülse (250) als einen oberen Längenabschnitt des Artikels und eine obere Oberfläche des Artikels formt.

8. Verfahren nach Anspruch 1, wobei die Außenschicht (260, 350) mehrere Außenschichten umfaßt.

9. Verfahren nach Anspruch 1, wobei der Artikel ein Vorformling (30, 330, 130, 160, 180) ist.

10. Verfahren nach Anspruch 9, wobei der erste Formungsschritt einen Halsabschnitt (250, 340, 190) des Vorformlings formt.

11. Verfahren nach Anspruch 10, wobei der Halsabschnitt aus einem Polymer geformt ist, das während des ersten Formungsschrittes kristallisiert.

12. Verfahren nach Anspruch 10, wobei der Halsabschnitt aus einem ersten Polymermaterial geformt wird, das einen höheren Einfrierpunkt hat als ein zweites Polymermaterial, das die Außenschicht formt.

13. Verfahren nach Anspruch 1, wobei die Hülse ein Gewicht in einem Bereich in der Größenordnung von 10-20%

des Gesamtgewichtes des Artikels hat.

14. Verfahren nach Anspruch 1, wobei die Hülse eine Wanddicke in einem Bereich in der Größenordnung von 0,5 bis 1,5 mm (0,02-0,06 inch) hat.
15. Verfahren nach Anspruch 14, wobei die Außenschicht eine Wanddicke in einem Bereich in der Größenordnung von 2,5-6,35 mm (0,10 - 0,25 inch) hat.
16. Verfahren nach Anspruch 1, wobei die Innenhülse aus einem ersten Material mit einer ersten Schmelztemperatur geformt ist und die Außenhülse eine zweite Schicht neben der Innenhülse umfaßt und aus einem zweiten Material geformt ist, das eine zweite Schmelztemperatur hat, die niedriger ist als die erste Schmelztemperatur.
17. Verfahren nach Anspruch 1, wobei der erste Formhohlraum (11) eine erste Hohlraumtemperatur hat und der zweite Formhohlraum (12) eine zweite Hohlraumtemperatur, die niedriger ist als die erste Hohlraumtemperatur.
18. Verfahren nach Anspruch 17, wobei der Kern (9) eine Kerntemperatur hat, die niedriger ist als die erste Hohlraumtemperatur.
19. Verfahren nach Anspruch 1, wobei die Innenhülse aus einem ersten Material mit einem ersten T_g geformt wird und die erhöhte Temperatur in einem Bereich in der Größenordnung von 5 - 20° C unterhalb des ersten T_g liegt.
20. Verfahren nach Anspruch 1, wobei die Hülse aus einem ersten Material geformt wird, das aus der Gruppe ausgewählt ist, die aus Homopolymeren, Copolymeren und Mischungen von Polyethylenphthalat (PEN) besteht.
21. Verfahren nach einem der Ansprüche 1 - 20, wobei die Außenschicht mindestens eine Schicht umfaßt, die aus einem zweiten Material geformt wurde, das aus der Gruppe ausgewählt wurde, die Polyethylenterephthalat (PET), ein Sauerstoffspülmateriale, wiederverwertetes PET, Polyethylen, Polypropylen, Polyacrylat, Polycarbonat, Polyacrylonitril, Nylon und Copolymere und Mischungen davon umfaßt.
22. Verfahren nach Anspruch 1, wobei der Artikel einen Seitenwandabschnitt aufweist, in dem die Innenhülse eine erste Dicke (t_1) hat und die Außenschicht eine zweite Dicke (t_2) und wobei das Verhältnis $t_2 : t_1$ größer ist als in der Größenordnung von 4 : 1.
23. Verfahren nach Anspruch 1, wobei der Artikel eine erste Dicke (t_1) hat und die Außenschicht eine zweite Dicke (t_2) und wobei das Verhältnis $t_2 : t_1$ in der Größenordnung von 1,2 : 1 bis 8 : 1 ist.
24. Verfahren nach Anspruch 1, wobei die Innenhülse (340) im wesentlichen kristallisiert ist und die Außenschicht (350) im wesentlichen amorph.
25. Verfahren nach Anspruch 1, wobei die Innenhülse aus einem ersten Material besteht und die Außenschicht aus einem zweiten Material und wobei das zweite Material eine niedrigere Kristallisationsrate als das erste Material hat.
26. Verfahren nach Anspruch 1, wobei erste und zweite Kerne (9, 10) bereitgestellt werden und wobei während eines ersten Zyklus' der erste Kern (9) im ersten Formhohlraum (11) angeordnet wird, um eine erste Innenhülse zu bilden, und der zweite Kern (10) mit einer zweiten darauf angeordneten Innenhülse gleichzeitig im zweiten Formhohlraum (12) angeordnet wird, um eine zweite Außenschicht auf der zweiten Innenhülse zu formen.
27. Verfahren nach Anspruch 26, wobei der erste Formungsschritt zu Beginn eine Ruheperiode umfaßt, während der zweite Formungsschritt voranschreitet, um die Übertragung zu ermöglichen, während die Außenfläche der Hülse eine angehobene Temperatur hat.
28. Verfahren nach Anspruch 1, wobei die Hülse aus einem ersten Material geformt ist, das aus der Gruppe ausgewählt ist, die aus Polyester, Polyester mit Keimbildnern, Acrylat, Polyethylenphthalat (PEN), Polycarbonat, Polypropylen, Polyamid, Polysulfon, Acrylonitrilstyren und Copolymeren und Mischungen davon besteht.
29. Verfahren nach Anspruch 28, wobei die Außenschicht ein zweites Material umfaßt, das aus der Gruppe ausgewählt ist, die aus Homopolymeren, Copolymeren und Mischungen aus einem oder mehreren der folgenden Stoffe besteht: Polyethylenterephthalat (PET), Polyethylenphthalat (PEN) und wiederverwertetes PET.

30. Verfahren nach Anspruch 1, wobei der Artikel (330) einen Körperabschnitt (350) hat und das Verfahren weiterhin ein Ausdehnen des Körperabschnittes des Artikels umfaßt, um einen ausgedehnten Artikel (270) mit einem im wesentlichen transparenten und biaxial orientierten Körperabschnitt (380) zu formen.
- 5 31. Verfahren nach Anspruch 1, wobei das Verfahren weiterhin ein Abkühlen des Artikels (330) unterhalb eines ersten Einfrierpunktes eines ersten Materials im Artikel umfaßt, ein Wiedererhitzen des Artikels über den ersten Einfrierpunkt und ein Ausdehnen des erhitzten Artikels, um einen ausgedehnten Artikel (270) zu formen.
- 10 32. Verfahren nach Anspruch 31, wobei der ausgedehnte Artikel (370) ein hohes T_g oder einen kristallisierten oberen Halsabschnitt (340) und einen im wesentlichen transparenten, biaxial orientierten Körperabschnitt (380) hat.
33. Vorrichtung zum Herstellen eines vielschichtigen spritzgeformten Kunststoffartikels, umfassend:
15 einen ersten Formhohlraum-Satz (11) und einen zweiten Formhohlraum-Satz (12), wobei der erste Formhohlraum angepaßt ist, um eine Innenhülssenschicht (20) zu formen, und der zweite Formhohlraum angepaßt ist, um eine Außenschicht (22) zu formen, wobei die Außenschicht (22) eine Dicke hat, die größer ist als die Dicke der Innenhülssenschicht (20);
einen Übergabemechanismus (2) mit ersten und zweiten Kern-Sätzen (9, 10) zum aufeinanderfolgenden Anordnen der ersten und zweiten Kern-Sätze in den ersten und zweiten Hohlraum-Sätzen;
20 wobei der erste Kern-Satz (9) im ersten Hohlraum-Satz (11) zum Formen eines Satzes von Innenhülssenschichten (20) auf dem ersten Kern-Satz angeordnet werden kann, während der zweite Kern-Satz (10) im zweiten Hohlraum-Satz (12) zum Formen eines zweiten Satzes von Außenschichten (22) über einen vorher geformten Satz von Innenhülssenschichten auf dem zweiten Kern-Satz angeordnet werden kann; und
25 eine Einrichtung zum Erhitzen des ersten Hohlraum-Satzes, um eine Außenfläche der Innenhülssenschicht (20) auf einer angehobenen Temperatur während der Übergabe und dem Formen der Außenschicht (22) darüber zu halten, wobei die angehobene Temperatur so gewählt ist, um Schmelzhaftung zwischen der Innenschicht und der Außenschicht zu erzielen.
- 30 34. Vorrichtung nach Anspruch 33, wobei der erste Formhohlraum (11) und Kern (9) eine erste Wanddicke (t_1) und der zweite Hohlraum (12) und Kern (10) eine zweite Wanddicke (t_2) definieren und wobei ein Verhältnis von $t_2 : t_1$ größer ist als in der Größenordnung von 4 : 1.
- 35 35. Vorrichtung nach Anspruch 33, wobei der Übergabemechanismus ein drehbarer Revolver (2) ist.
36. Vorrichtung nach Anspruch 33, wobei der Übergabemechanismus ein sich hin- und herbewegender Wagen (206) ist.
37. Vorrichtung nach Anspruch 33, umfassend eine Einrichtung, mit der das Formen der Außenschichten im zweiten Hohlraum-Satz in Gang gesetzt wird, während im ersten Hohlraum-Satz eine Ruheperiode aufrechterhalten wird, um die Übergabe zu ermöglichen, während die Außenfläche der Hülssenschicht die angehobene Temperatur hat.
- 40 38. Verfahren nach Anspruch 1, umfassend:
45 Spritzformen eines ersten thermoplastischen Materials, um einen ersten Vorformlingsabschnitt (340) mit einer Innenhülssenschicht (20) zu formen, die eine durchschnittliche prozentuale Kristallinität von mindestens ungefähr 30% hat; und
Spritzformen eines zweiten thermoplastischen Materials, um einen zweiten Vorformlingsabschnitt (350) mit einer Außenhülse (22) zu formen, die im wesentlichen amorph bleibt.
- 50 39. Verfahren nach Anspruch 38, wobei der erste Abschnitt im wesentlichen ein Halsabschnitt (340) ist und der zweite Abschnitt im wesentlichen ein körperlbildender Abschnitt (350).
40. Verfahren nach Anspruch 38, wobei das zweite Material eine niedrigere Kristallisationsrate hat als das erste Material.
- 55 41. Verfahren nach Anspruch 40, wobei das erste Material aus der Gruppe ausgewählt ist, die aus Polyester, Polyester mit Keimbildern, Acrylatpolymeren, Polyethylenaphthalat (PEN), Polycarbonat, Polypropylen, Polyamid, Polysulfon, Acrylonitrilstyren und Copolymere und Mischungen davon besteht.

42. Verfahren nach Anspruch 41, wobei das zweite Material aus der Gruppe ausgewählt ist, die aus Homopolymeren, Copolymeren und Mischungen aus einem oder mehreren der folgenden Stoffe besteht: Polyethylenterephthalat (PET), Polyethylenphthalat (PEN) und wiederverwertetes PET.
- 5 43. Verfahren nach Anspruch 41, weiterhin umfassend ein Ausdehnen des zweiten Abschnittes (350), um einen im wesentlichen transparenten und biaxial orientierten Körper (380) eines Behälters (340) zu formen.
44. Verfahren nach Anspruch 1, umfassend:
 - 10 zuerst Formen der Innenhölse (20) auf einem Kern (9), der in einem ersten Formhohlraum (11) angeordnet ist, wobei der erste Formungsschritt ein Füllstadium und ein Druck-Stoß-Stadium umfaßt, aber im wesentlichen kein Halte- und Kühl-Stadium, damit die Außenfläche der Innenhölse für einen zweiten Formungsschritt auf einer angehobenen Temperatur gehalten wird;
 - 15 Entfernen der Hölse (20) auf dem Kern (9) und Übergeben derselben ohne wesentliche Verzögerung an den zweiten Formhohlraum (12); und
 - zweites Formen der Außenschicht (22) über der Hölse (20) im zweiten Formhohlraum (12), um den vielschichtigen spritzgeformten Artikel zu formen.
45. Verfahren nach Anspruch 1, wobei die Innenhölse aus einem PEN-Polymer-Material hergestellt ist und die angehobene Temperatur in einem Bereich in der Größenordnung von 60 - 120° C liegt.
- 20 46. Verfahren nach Anspruch 45, wobei der erste Formungsschritt eine Zyklusdauer in der Größenordnung von nicht mehr als 8 Sekunden hat.
- 25 47. Verfahren nach Anspruch 45, wobei die Zyklusdauer in einem Bereich in der Größenordnung von 4-8 Sekunden liegt.
48. Verfahren nach Anspruch 45, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 40 - 120° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 5 - 80° C.
- 30 49. Verfahren nach Anspruch 48, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 75 - 95° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 60 - 70° C.
50. Verfahren nach Anspruch 48, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 100 - 110° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 5 - 15° C.
- 35 51. Verfahren nach Anspruch 48, wobei das PEN-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 275 - 295° C hat und die angehobene Temperatur in einem Bereich in der Größenordnung von 90 - 110° C liegt.
- 40 52. Verfahren nach Anspruch 1, wobei die Außenschicht ein PET-Polymer-Material neben der Innenhölse umfaßt, wobei das PET-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 260 - 275° C hat und der zweite Formungsschritt bei einem Hohlraumdruck in einem Bereich in der Größenordnung von 55×10^6 bis 103×10^6 N/m² (8000- 15000 psi) ausgeführt wird.
- 45 53. Verfahren nach Anspruch 1, wobei die Innenhölse aus einem Polyester-Polymer-Material hergestellt wird, das während des ersten Formungsschrittes kristallisiert ist, und wobei die angehobene Temperatur in einem Bereich in der Größenordnung von 80 - 140° C liegt.
- 50 54. Verfahren nach Anspruch 53, wobei der erste Formungsschritt eine Zyklusdauer in der Größenordnung von nicht mehr als 8 Sekunden hat.
- 55 55. Verfahren nach Anspruch 54, wobei die Zyklusdauer in einem Bereich in der Größenordnung von 5-8 Sekunden liegt.
56. Verfahren nach Anspruch 53, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 80 - 150° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung 5 - 60° C.

57. Verfahren nach Anspruch 56, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 110 - 120° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung 5 - 15° C.

58. Verfahren nach Anspruch 53, wobei das Polyester-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 280 - 290° C hat und die angehobene Temperatur in einem Bereich in der Größenordnung von 115-125° C liegt.

59. Verfahren nach Anspruch 53, wobei die Außenschicht ein PET-Polymer-Material neben der Innenhülse umfaßt, wobei das PET-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 270 - 285°C hat und der zweite Formungsschritt bei einem Hohlraumdruck in einem Bereich in der Größenordnung von 55×10^6 bis 103×10^6 N/m² (8000- 15000 psi) ausgeführt wird.

60. Verfahren nach Anspruch 44, wobei:

die Innenhülse aus einem PEN-Polymer-Material hergestellt wird;
während des zweiten Formungsschrittes die Außenfläche der Hülse eine angehobene Temperatur in einem Bereich in der Größenordnung von 100-110° C hat und die Außenschicht eine erste Außenschicht aus einem PET-Polymer-Material neben der Innenhülse umfaßt, und wobei das PET-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 260 - 275°C hat und der zweite Formungsschritt bei einem Hohlraumdruck in einem Bereich in der Größenordnung von 55×10^6 bis 103×10^6 N/m² (8000- 15000 psi) ausgeführt wird, um eine Schmelzhaftung zwischen der Innenhülse und der Außenschicht während des zweiten Formungsschrittes zu erzielen.

61. Verfahren nach Anspruch 44, wobei:

eine Innenhülse aus einem PEN-Polymer-Material geformt ist;
während des zweiten Formungsschrittes die Außenfläche der Hülse eine angehobene Temperatur in einem Bereich in der Größenordnung von 90-100° C hat und die Außenschicht eine erste Außenschicht aus einem PET-Polymer-Material neben der Innenhülse umfaßt, und wobei das PET-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 260 - 275°C hat und der zweite Formungsschritt bei einem Hohlraumdruck in einem Bereich in der Größenordnung von 55×10^6 bis 103×10^6 N/m² (8000 - 15000 psi) ausgeführt wird, um eine Schmelzhaftung zwischen der Innenhülse und der Außenschicht während des zweiten Formungsschrittes zu erzielen.

62. Verfahren nach Anspruch 44, wobei:

die Innenhülse aus einem Polyester-Polymer-Material hergestellt ist, das auf dem Kern während des ersten Formungsschrittes kristallisiert ist; und
während des zweiten Formungsschrittes die Außenfläche der Hülse eine angehobene Temperatur in einem Bereich in der Größenordnung von 115-125° C hat und die Außenschicht eine erste Außenschicht aus einem PET-Polymer-Material neben der Innenhülse hat und wobei das PET-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 270 - 285°C hat und der zweite Formungsschritt bei einem Hohlraumdruck in einem Bereich in der Größenordnung von 55×10^6 bis 103×10^6 N/m² (8000-15000 psi) ausgeführt wird, um eine Schmelzhaftung zwischen der Innenhülse und der Außenschicht während des zweiten Formungsschrittes zu erzielen.

63. Verfahren nach einem der Ansprüche 44, 60, 61 und 62, wobei die Hülse ein Gewicht in einem Bereich in der Größenordnung von 10 - 20% des Gesamtgewichtes des Artikels hat.

64. Verfahren nach einem der Ansprüche 44, 60, 61 und 62, wobei die Hülse eine Wanddicke in einem Bereich in der Größenordnung von 0,5 - 1,5 mm (0,02-0,06 inch) hat.

65. Verfahren nach einem der Ansprüche 44, 60, 61, 62 und 64, wobei die Außenschicht eine Wanddicke in einem Bereich in der Größenordnung von 2,50-6,35 mm (0,10 - 0,25 inch) hat.

66. Verfahren nach Anspruch 44, wobei die Innenhülse aus einem PEN-Polymer-Material hergestellt ist und die angehobene Temperatur in einem Bereich in der Größenordnung von 60 - 120° C liegt.

67. Verfahren nach Anspruch 44, wobei der erste Formungsschritt eine Zyklusdauer in der Größenordnung von nicht mehr als 8 Sekunden hat.
- 5 68. Verfahren nach Anspruch 44, wobei die Zyklusdauer in einem Bereich in der Größenordnung von 4 - 8 Sekunden liegt.
69. Verfahren nach Anspruch 44, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 40 - 120° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 5 - 8° C.
- 10 70. Verfahren nach Anspruch 69, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 75 - 95° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 60 - 70° C.
- 15 71. Verfahren nach Anspruch 69, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 100 - 110° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 5 - 15° C.
72. Verfahren nach Anspruch 66, wobei das PEN-Polymer-Material eine Schmelztemperatur in einem Bereich von 270 - 295° C hat und die angehobene Temperatur in einem Bereich in der Größenordnung von 90 - 110° C liegt.
- 20 73. Verfahren nach Anspruch 66, wobei die Außenschicht ein PET-Polymer-Material neben der Innenhülse umfaßt, wobei das PET-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 260 - 275° C hat und der zweite Formungsschritt bei einem Hohlraumdruck in einem Bereich in der Größenordnung von 55×10^6 bis 103×10^6 N/m² (8000- 15000 psi) ausgeführt wird.
- 25 74. Verfahren nach Anspruch 44, wobei die Innenhülse aus einem Polyester-Polymer-Material hergestellt wird, das während des ersten Formungsschrittes kristallisiert ist, und die angehobene Temperatur in einem Bereich in der Größenordnung von 80 - 140° C liegt.
75. Verfahren nach Anspruch 74, wobei der erste Formungsschritt eine Zyklusdauer in der Größenordnung von nicht mehr als 8 Sekunden hat.
- 30 76. Verfahren nach Anspruch 74, wobei der erste Formungsschritt eine Zyklusdauer in der Größenordnung von 5-8 Sekunden liegt.
- 35 77. Verfahren nach Anspruch 74, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 80 - 150° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 5 - 60° C.
78. Verfahren nach Anspruch 77, wobei die erste Hohlraumtemperatur in einem Bereich in der Größenordnung von 110 - 120° C liegt und die Kerntemperatur in einem Bereich in der Größenordnung von 5 - 15° C.
- 40 79. Verfahren nach Anspruch 74, wobei das Polyester-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 280 - 290° C hat und die angehobene Temperatur in einem Bereich in der Größenordnung von 115-125° C liegt.
- 45 80. Verfahren nach Anspruch 74, wobei die Außenschicht ein PET-Polymer-Material neben der Innenhülse umfaßt, wobei das PET-Polymer-Material eine Schmelztemperatur in einem Bereich in der Größenordnung von 270 - 285° C hat und der zweite Formungsschritt bei einem Hohlraumdruck in einem Bereich in der Größenordnung von 55×10^6 bis 103×10^6 N/m² (8000- 15000 psi) ausgeführt wird.

50 Revendications

1. Procédé de réduction de l'épaisseur d'une couche intérieure et d'amélioration de l'adhérence d'une couche dans un article multicouche en matière plastique moulé par injection, le procédé comportant les étapes consistant à :
55 tout d'abord mouler une couche de manchon intérieur (20) entre une première cavité de moule (11) et un noyau (9), la première cavité de moule étant chauffée pour maintenir une surface extérieure de la couche de manchon intérieur à une température élevée, transférer le noyau (9) et la couche de manchon (1) vers une seconde cavité de moule (12) et deuxièmement

mouler une couche extérieure (22) sur la couche de manchon alors que la surface extérieure est à la température élevée, la couche extérieure (22) ayant une épaisseur plus grande que l'épaisseur de la couche de manchon intérieur (20), la température élevée étant sélectionnée pour fournir une adhérence par fusion entre le manchon intérieur (20) et la couche extérieure (22) pendant la seconde étape de moulage.

2. Procédé selon la revendication 1, dans lequel l'adhérence par fusion entre le manchon intérieur (20) et la couche extérieure (22) comporte une fixation par diffusion.
3. Procédé selon la revendication 1, dans lequel l'adhérence par fusion entre le manchon intérieur (20) et la couche extérieure (22) comporte un enchevêtrement de chaîne.
4. Procédé selon la revendication 1, dans lequel le manchon forme une partie de manchon supérieure (250, 340, 190) de l'article, et la couche extérieure forme une partie de corps inférieure (260, 350, 180) de l'article.
5. Procédé selon la revendication 4, dans lequel une extrémité inférieure de la partie de manchon supérieure et une extrémité supérieure de la partie de corps inférieure sont reliées dans une partie intermédiaire de l'article.
6. Procédé selon la revendication 1, dans lequel la première étape de moulage forme le manchon intérieur (120, 170) sous la forme d'une couche intérieure sur toute la longueur (121, 171) et d'une surface supérieure (122, 172) de l'article.
7. Procédé selon la revendication 1, dans lequel la première étape de moulage forme le manchon intérieur (250) sous la forme d'une partie de longueur supérieure de l'article et d'une surface supérieure de l'article.
8. Procédé selon la revendication 1, dans lequel la couche extérieure (260, 350) est constituée de multiples couches extérieures.
9. Procédé selon la revendication 1, dans lequel l'article est une préforme (30, 330, 130, 160, 180).
10. Procédé selon la revendication 9, dans lequel la première étape de moulage forme une partie finie formant col (250, 340, 190) de la préforme.
11. Procédé selon la revendication 10, dans lequel la partie finie formant col est moulée à partir d'un polymère qui cristallise pendant la première étape de moulage.
12. Procédé selon la revendication 10, dans lequel la partie finie formant col est moulée à partir d'un premier polymère ayant une température de transition vitreuse plus élevée qu'un second polymère qui forme la couche extérieure.
13. Procédé selon la revendication 1, dans lequel le manchon a un poids situé dans une plage allant de 10 à 20 pourcent du point total de l'article.
14. Procédé selon la revendication 1, dans lequel le manchon a une épaisseur de paroi située dans la plage allant de 0,5 à 1,5 mm (0,02 à 0,06 pouce).
15. Procédé selon la revendication 14, dans lequel la couche extérieure a une épaisseur de paroi située dans la plage allant de 2,50 à 6,35 mm (0,10 à 0,25 pouce).
16. Procédé selon la revendication 1, dans lequel le manchon intérieur est formé d'un premier matériau ayant une première température de fusion, et la couche extérieure comporte une seconde couche adjacente au manchon intérieur et constituée d'un second matériau ayant une seconde température de fusion inférieure à la première température de fusion.
17. Procédé selon la revendication 1, dans lequel la première cavité de moule (11) est à une première température de cavité et la seconde cavité de moule (12) est à une seconde température de cavité plus basse que la première température de cavité.
18. Procédé selon la revendication 17, dans lequel le noyau (9) est à une température de noyau qui est plus petite que la première température de cavité.

19. Procédé selon la revendication 1, dans lequel le manchon intérieur est formé d'un premier matériau ayant une première T_g et la température élevée est dans une plage allant de 5 à 20°C en dessous de la première T_g .
20. Procédé selon la revendication 1, dans lequel le manchon est moulé à partir d'un premier matériau sélectionné parmi le groupe constitué d'homopolymères, copolymères, et de mélanges de polyéthylène naphthalate (PEN).
21. Procédé selon l'une quelconque des revendications 1 et 20, dans lequel la couche extérieure comporte au moins une couche moulée à partir d'un second matériau sélectionné parmi le groupe constitué de polyéthylène téréphthalate (PET), d'un matériau d'épuration de l'oxygène, de PET recyclé, de polyéthylène, de polypropylène, de polyacrylate, de polycarbonate, de polyacrylonitrile, de Nylon, et de copolymères et de mélanges de ceux-ci.
22. Procédé selon la revendication 1, dans lequel l'article a une partie de paroi latérale dans laquelle le manchon intérieur a une première épaisseur (t_1) et la couche extérieure a une seconde épaisseur (t_2), et le rapport $t_2:t_1$ est plus grand que 4:1.
23. Procédé selon la revendication 1, dans lequel l'article a une première épaisseur (t_1) et la couche extérieure a une seconde épaisseur (t_2), et le rapport $t_2:t_1$ est de l'ordre de 1,2:1 à 8:1.
24. Procédé selon la revendication 1, dans lequel le manchon intérieur (340) est pratiquement cristallisé et la couche extérieure (360) est pratiquement amorphe.
25. Procédé selon la revendication 1, dans lequel le manchon intérieur est constitué d'un premier matériau et la couche extérieure est constituée d'un second matériau, et le second matériau a un taux de cristallisation inférieur par comparaison au premier matériau.
26. Procédé selon la revendication 1, dans lequel des premier et second noyaux (9, 10) sont fournis, et dans lequel pendant un premier cycle le premier noyau (9) est positionné dans une première cavité de moule (11) pour former un premier manchon intérieur, et le second noyau (10) ayant un second manchon intérieur positionné sur celui-ci, est positionné simultanément dans la seconde cavité de moule (12) pour mouler une seconde couche extérieure sur le second manchon intérieur.
27. Procédé selon la revendication 26, dans lequel la première étape de moulage comporte une période initiale sans action lorsque la seconde étape de moulage est faite pour faciliter le transfert alors que la surface extérieure de la couche de manchon est à une température élevée.
28. Procédé selon la revendication 1, dans lequel le manchon est moulé d'un premier matériau sélectionné parmi le groupe constitué de polyesters, de polyesters ayant des agents de nucléation, d'acrylate, de polyéthylène naphthalate (PEN), de polycarbonate, de polypropylène, de polyamide, de polysulfone, de styrène-acrylonitrile, et de copolymères et de mélanges de ceux-ci.
29. Procédé selon la revendication 28, dans lequel la couche intérieure comporte un second matériau sélectionné parmi le groupe constitué d'homopolymères, de copolymères, et de mélanges d'un ou plusieurs parmi : polyéthylène téréphthalate (PET), polyéthylène naphthalate (PEN), et PET recyclé.
30. Procédé selon la revendication 1, dans lequel l'article (330) a une partie de corps (350) et le procédé comporte en outre l'expansion de la partie de corps de l'article pour former un article expansé (70) ayant une partie de corps sensiblement transparente et orientée biaxialement (380).
31. Procédé selon la revendication 1, dans lequel le procédé comporte en outre le refroidissement de l'article (330) en dessous d'une première température de transition vitreuse d'un premier matériau de l'article, le réchauffage de l'article au-dessus de la première température de transition vitreuse, et l'expansion de l'article réchauffé pour former un article expansé (370).
32. Procédé selon la revendication 31, dans lequel l'article expansé (370) a une T_g élevée ou une partie finie formant col supérieur cristallisée (340) et une partie de corps sensiblement transparente, orientée biaxialement (380).
33. Dispositif pour fabriquer des articles en matière plastique moulés par injection, à plusieurs couches comportant :

un ensemble de premières cavités de moule (11) et un ensemble de secondes cavités de moule (12), chaque première cavité étant adaptée pour former une couche de manchon inférieur (20) et chaque seconde cavité étant adaptée pour former une couche extérieure (22), la couche extérieure (22) ayant une épaisseur plus grande que l'épaisseur de la couche de manchon inférieur (20).

un mécanisme de transfert (2) ayant des ensembles de premiers et seconds noyaux (9, 10) pour positionner successivement les ensembles de premiers et seconds noyaux dans les ensembles de premières et secondes cavités,

dans lequel l'ensemble de premiers noyaux (9) peut être positionné dans l'ensemble de premières cavités (11) pour mouler un ensemble de couches de manchon inférieur (20) sur l'ensemble de premiers noyaux, alors que l'ensemble de seconds noyaux (10) peut être positionné dans l'ensemble de secondes cavités (12) pour mouler sur un ensemble au préalable de couches de manchon inférieur situé sur l'ensemble de seconds noyaux, un second ensemble de couches extérieures (22), et

des moyens pour chauffer (15) l'ensemble de premières cavités de manière à maintenir la surface extérieure de la couche de manchon inférieur (20) à une température élevée pendant le transfert et le moulage de la couche extérieure (22) sur celle-ci, la température élevée étant sélectionnée pour fournir une adhérence par fusion entre le manchon inférieur et la couche extérieure.

34. Dispositif selon la revendication 33, dans lequel la première cavité (11) et le noyau (9) définissent une première épaisseur de paroi (t_1) et la seconde cavité (12) et le noyau (10) définissent une seconde épaisseur de paroi (t_2), et dans lequel le rapport $t_2:t_1$ est plus grand que 4:1.

35. Dispositif selon la revendication 33, dans lequel le mécanisme de transfert est une tourelle rotative (2).

36. Dispositif selon la revendication 33, dans lequel le mécanisme de transfert est une navette se déplaçant en va et vient (206).

37. Dispositif selon la revendication 33, comportant des moyens pour déclencher le moulage des couches extérieures dans l'ensemble de secondes cavités tout en maintenant une période sans action dans l'ensemble de premières cavités afin de faciliter le transfert alors que la surface extérieure de la couche de manchon est à la température élevée.

38. Procédé selon la revendication 1, comportant :

le moulage par injection d'un premier matériau thermoplastique pour former une première partie de préforme (340) incluant la couche de manchon inférieur (20) ayant un pourcentage de cristallinité moyen d'au moins environ 30 %, et

mouler par injection un second matériau thermoplastique pour former une seconde partie de préforme (350) incluant le manchon extérieur (22) qui reste pratiquement amorphe.

39. Procédé selon la revendication 38, dans lequel la première partie est sensiblement une partie de col (340) et la seconde partie est sensiblement une partie de formation de corps (350).

40. Procédé selon la revendication 38, dans lequel le second matériau a un taux de cristallisation inférieur par comparaison au premier matériau.

41. Procédé selon la revendication 40, dans lequel le premier matériau est sélectionné parmi le groupe constitué de polyester, de polyester ayant des agents de nucléation, de polymères d'acrylate, de polyéthylène naphthalate (PEN), de polycarbonate, de polypropylène, de polyamide, de polysulfone, de styrène-acrylonitrile, et de copolymères et de mélanges de ceux-ci.

42. Procédé selon la revendication 41, dans lequel le second matériau est sélectionné parmi le groupe constitué d'homopolymères, de copolymères et de mélanges de l'un ou plusieurs parmi du polyéthylène téréphtalate (PET), du polyéthylène naphthalate (PEN), et du PET recyclé.

43. Procédé selon la revendication 41, comportant de plus l'expansion de la seconde partie (350) pour former un corps sensiblement transparent et orienté biaxialement (380) d'un conteneur (370).

44. Procédé selon la revendication 1, comportant les étapes consistant à :

- 5 tout d'abord mouler le manchon intérieur (20) sur un noyau (9) positionné dans la première cavité de moule (11), la première étape de moulage comportant un étage de remplissage et un étage de mise en pression mais pratiquement pas d'étage de maintien et de refroidissement de manière à maintenir la surface extérieure du manchon intérieur à une température élevée pour une seconde étape de moulage, enlever le manchon (20) situé sur le noyau (9) mais transférer celui-ci sans retard important vers la seconde cavité de moule (12), et deuxièmement mouler la couche extérieure (22) sur le manchon (20) situé dans la seconde cavité de moule (12) pour former l'article moulé par injection à plusieurs couches.
- 10 45. Procédé selon la revendication 1, dans lequel le manchon intérieur est constitué d'un polymère de PEN et la température élevée est dans la plage allant de 60 à 120°C.
- 15 46. Procédé selon la revendication 45, dans lequel la première étape de moulage a un temps de cycle qui n'est pas plus grand que 8 secondes.
47. Procédé selon la revendication 45, dans lequel le temps de cycle est dans la plage allant de 4 à 8 secondes.
- 20 48. Procédé selon la revendication 45, dans lequel la température de première cavité est dans la plage allant de 40 à 120°C et la température de noyau est dans la plage allant de 5 à 80°C environ.
49. Procédé selon la revendication 48, dans lequel la température de première cavité est dans la plage allant de 75 à 95°C environ et la température de noyau est dans la plage allant de 60 à 70°C environ.
- 25 50. Procédé selon la revendication 48, dans lequel la température de première cavité est dans la plage allant de 100 à 110°C environ et la température de noyau est dans la plage allant de 5 à 15°C environ.
51. Procédé selon la revendication 48, dans lequel le polymère de PEN a une température de fusion dans la plage allant de 275 à 295°C environ et la température élevée est dans la plage allant de 90 à 110°C environ.
- 30 52. Procédé selon la revendication 1, dans lequel la couche extérieure comporte un polymère de PET adjacent au manchon intérieur, le polymère de PET ayant une température de fusion située dans la plage allant de 260 à 275°C environ et la seconde étape de moulage est effectuée à une pression de cavité dans la plage allant de 55×10^6 à 103×10^6 N/m² (8 000 à 15 000 psi),
- 35 53. Procédé selon la revendication 1, dans lequel le manchon intérieur est constitué de polymère de polyester qui est cristallisé pendant la première étape de moulage et la température élevée est dans la plage allant de 80 à 140°C environ.
- 40 54. Procédé selon la revendication 53, dans lequel la première étape de moulage a un temps de cycle qui n'est pas plus grand que 8 secondes.
- 55 55. Procédé selon la revendication 45, dans lequel le temps de cycle est dans la plage allant de 4 à 8 secondes.
56. Procédé selon la revendication 55, dans lequel la température de première cavité est dans la plage allant de 8 à 150°C et la température de noyau est dans la plage allant de 5 à 60°C environ.
57. Procédé selon la revendication 56, dans lequel la température de première cavité est dans la plage allant de 110 à 120°C environ et la température de noyau est dans la plage allant de 5 à 15°C environ.
- 50 58. Procédé selon la revendication 53, dans lequel le polymère de polyester a une température de fusion située dans la plage allant de 280 à 290°C environ et la température élevée est dans la plage allant de 115 à 125°C environ.
59. Procédé selon la revendication 53, dans lequel la couche extérieure est constituée de polymère de PET ayant une température de fusion située dans la plage allant de 270 à 285°C environ et la seconde étape de moulage est effectuée à une pression de cavité située dans la plage allant de 55×10^6 à 103×10^6 N/m² environ (8 000 à 15 000 psi)
60. Procédé selon la revendication 44, dans lequel :

le manchon intérieur est en polymère de PEN

pendant la seconde étape de moulage la surface extérieure du manchon est à une température élevée située dans une plage allant de 90 à 100°C environ et la couche extérieure comporte une première couche extérieure de polymère de PET adjacente au manchon intérieur, et dans lequel le polymère de PET a une température de fusion située dans une plage allant de 260 à 275°C environ et la seconde étape de moulage est effectuée à une pression de cavité située dans une plage allant de 55×10^6 à 103×10^6 N/m² (8 000 à 15 000 psi) pour obtenir une adhérence par fusion entre le manchon intérieur et la couche extérieure pendant la seconde étape de moulage.

61. Procédé selon la revendication 44, dans lequel :

un manchon intérieur est constitué de polymère de PEN moulé

pendant la seconde étape de moulage la surface extérieure du manchon est à une température élevée située dans une plage allant de 90 à 100°C environ et la couche extérieure comporte une première couche extérieure de polymère de PET adjacente au manchon intérieur, et le polymère de PET a une température de fusion située dans une plage allant de 260 à 275°C environ et la seconde étape de moulage est effectuée à une pression de cavité située dans une plage allant de 55×10^6 à 103×10^6 N/m² (8 000 à 15 000 psi) pour aboutir à une adhérence par fusion entre le manchon intérieur et la couche extérieure pendant la seconde étape de moulage.

62. Procédé selon la revendication 44, dans lequel :

le manchon intérieur est constitué de polymère de polyester qui est cristallisé sur le noyau pendant la première étape de moulage, et

pendant la seconde étape de moulage la surface extérieure du manchon est à une température élevée située dans une plage allant de 115 à 125°C environ et la couche extérieure comporte une première couche extérieure de polymère de PET adjacente au manchon intérieur, et le polymère de PET a une température de fusion située dans une plage allant de 270 à 285°C environ et la seconde étape de moulage est effectuée à une pression de cavité située dans une plage allant de 55×10^6 à 103×10^6 N/m² (8 000 à 15 000 psi) pour aboutir à une adhérence par fusion entre le manchon intérieur et la couche extérieure pendant la seconde étape de moulage.

63. Procédé selon l'une quelconque des revendications 44, 60, 61 et 62, dans lequel le manchon a un poids situé dans une plage allant de 10 à 20 pourcent environ du poids total de l'article.

64. Procédé selon l'une quelconque des revendications 44, 60, 61 et 62, dans lequel le manchon a une épaisseur de paroi située dans une plage allant de 0,5 à 1,5 mm (0,02 à 0,06 pouce).

65. Procédé selon l'une quelconque des revendications 44, 60, 61, 62 et 64, dans lequel la couche extérieure a une épaisseur de paroi située dans une plage allant de 2,50 à 6,35 mm (0,10 à 0,25 pouce).

66. Procédé selon la revendication 44, dans lequel le manchon intérieur est constitué d'un polymère de PEN et la température élevée est dans une plage allant de 60 à 120°C environ.

67. Procédé selon la revendication 44, dans lequel la première étape de moulage a un temps de cycle qui n'est pas plus grand qu'environ 8 secondes.

68. Procédé selon la revendication 44, dans lequel le temps de cycle est dans une plage allant de 4 à 8 secondes environ.

69. Procédé selon la revendication 44, dans lequel la température de première cavité est dans une plage allant de 40 à 120°C environ et la température de noyau est dans une plage allant de 5 à 80°C environ.

70. Procédé selon la revendication 69, dans lequel la température de première cavité est dans une plage allant de 75 à 95°C environ et la température de noyau est dans une plage allant de 60 à 70°C environ.

71. Procédé selon la revendication 69, dans lequel la température de première cavité est dans une plage allant de 100 à 110°C environ et la température de noyau est dans une plage allant de 5 à 15°C environ.

72. Procédé selon la revendication 66, dans lequel le polymère de PEN a une température de fusion située dans une plage allant de 275 à 295°C environ et la température élevée est dans une plage allant de 90 à 110°C environ.
- 5 73. Procédé selon la revendication 66, dans lequel la couche intérieure est en polymère de PET, adjacente au manchon intérieur, le polymère de PET ayant une température de fusion située dans une plage allant de 260 à 275°C environ et la seconde étape de moulage est effectuée à une pression de cavité située dans une plage allant de 55×10^6 à 103×10^6 N/m² (8 000 à 15 000 psi).
- 10 74. Procédé selon la revendication 44, dans lequel le manchon intérieur est constitué d'un polymère de polyester qui est cristallisé pendant la première étape de moulage et la température élevée est dans la plage allant de 80 à 140°C environ.
- 15 75. Procédé selon la revendication 74, dans lequel la première étape de moulage a un temps de cycle qui n'est pas plus grand que 8 secondes environ.
- 20 76. Procédé selon la revendication 74, dans lequel le temps de cycle est dans une plage allant de 5 à 8 secondes environ.
77. Procédé selon la revendication 74, dans lequel la température de première cavité est dans une plage allant de 80 à 150°C environ et la température de noyau est dans une plage allant de 5 à 60°C.
78. Procédé selon la revendication 77, dans lequel la température de première cavité est dans une plage allant de 110 à 120°C environ et la température de noyau est dans une plage allant de 5 à 15°C environ.
- 25 79. Procédé selon la revendication 74, dans lequel le polymère de polyester a une température de fusion située dans une plage allant de 280 à 290°C environ et la température élevée est dans une plage allant de 115 à 125°C environ.
- 30 80. Procédé selon la revendication 74, dans lequel la couche extérieure comporte un polymère de PET adjacent au manchon intérieur, le polymère de PET ayant une température de fusion située dans une plage allant de 270 à 285°C environ et la seconde étape de moulage est effectuée à une pression de cavité située dans une plage allant de 55×10^6 à 103×10^6 N/m² (8 000 à 15 000 psi).

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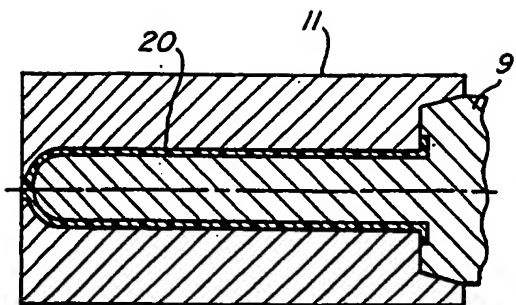


Fig. 1A

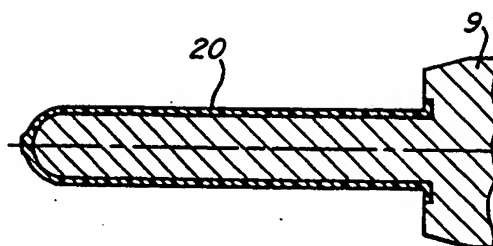


Fig. 1B

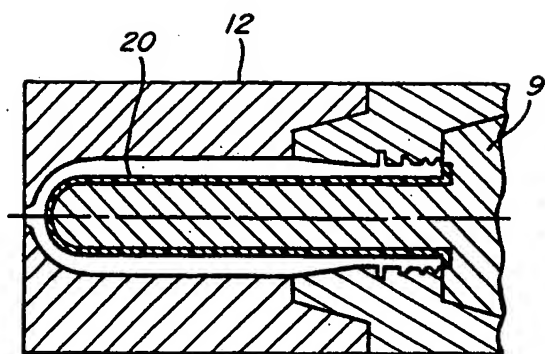


Fig. 1C

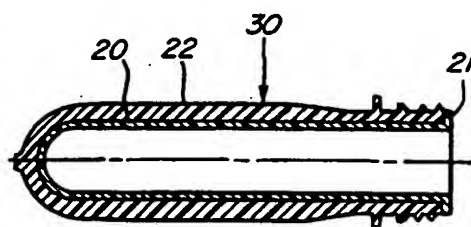


Fig. 1D

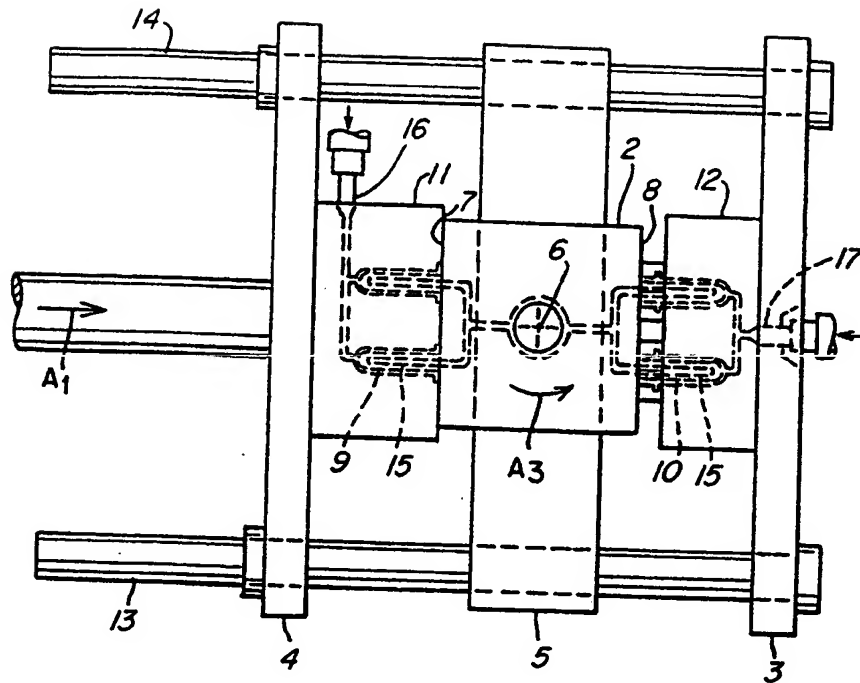


Fig. 2A

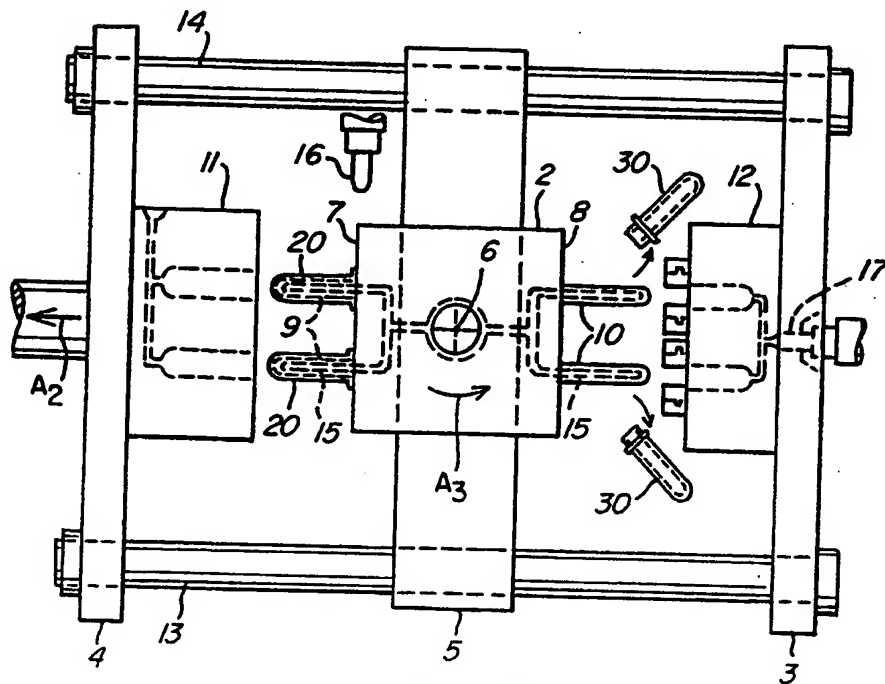


Fig. 2B

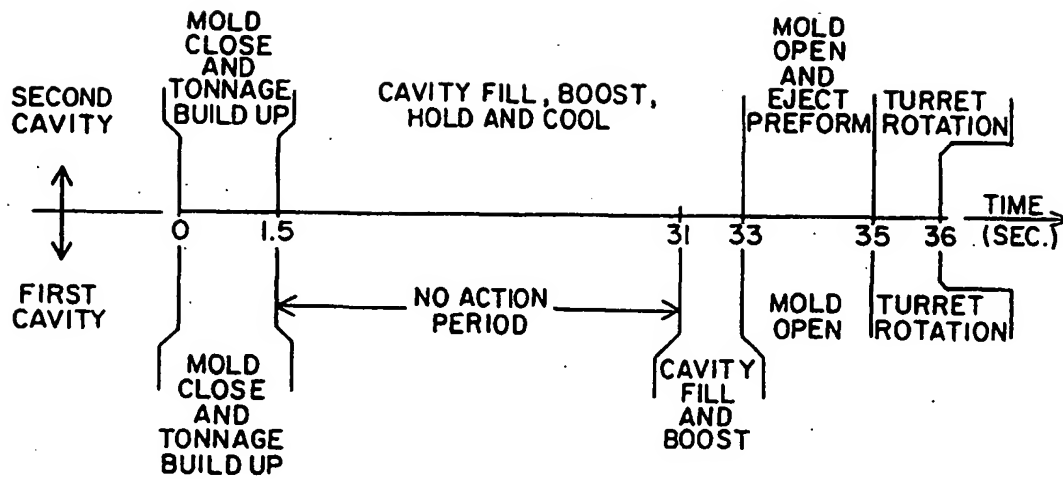


Fig. 3

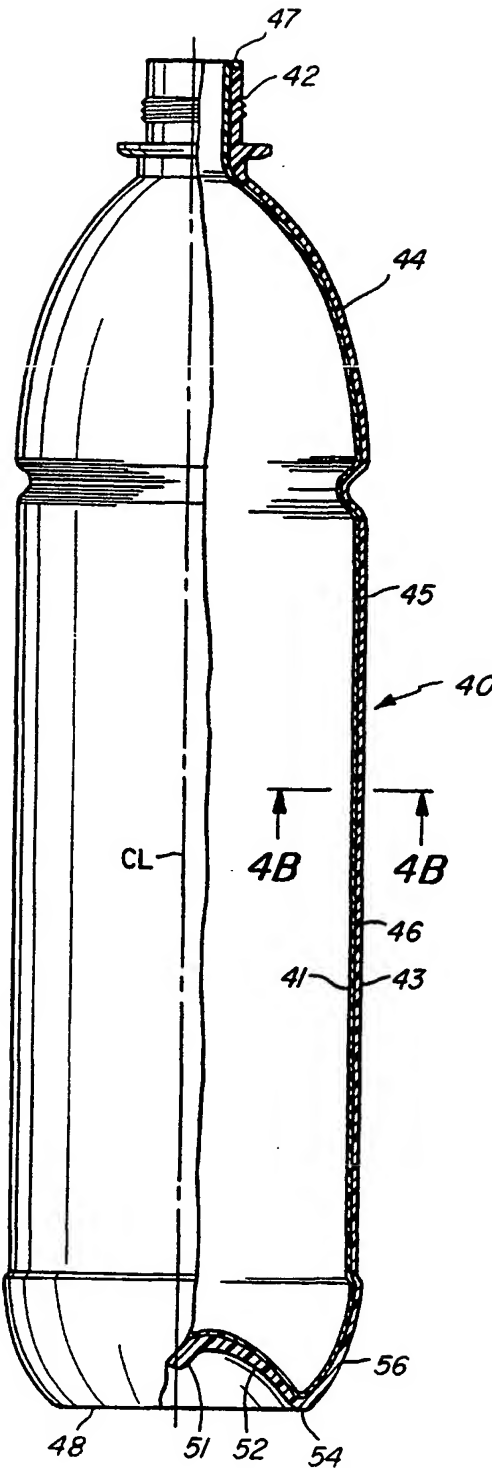


Fig. 4A

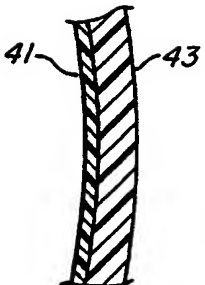


Fig. 4B

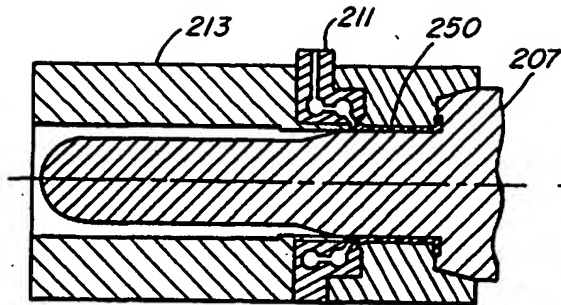


Fig. 5A

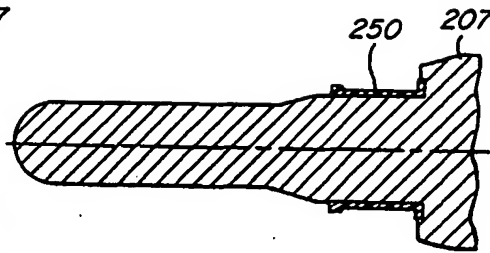


Fig. 5B

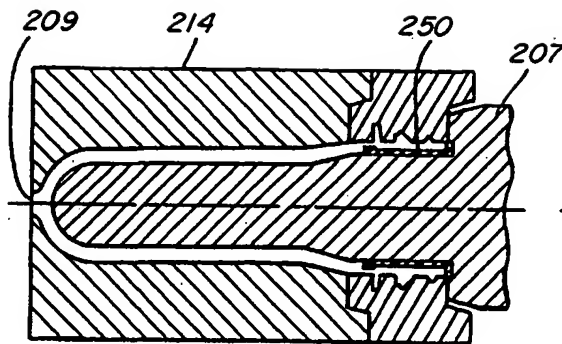


Fig. 5C

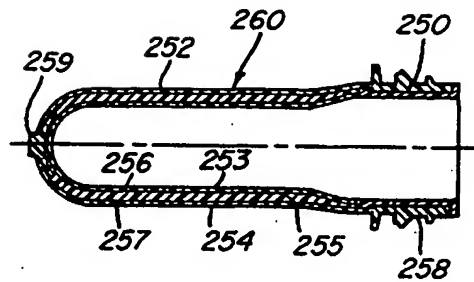


Fig. 5D

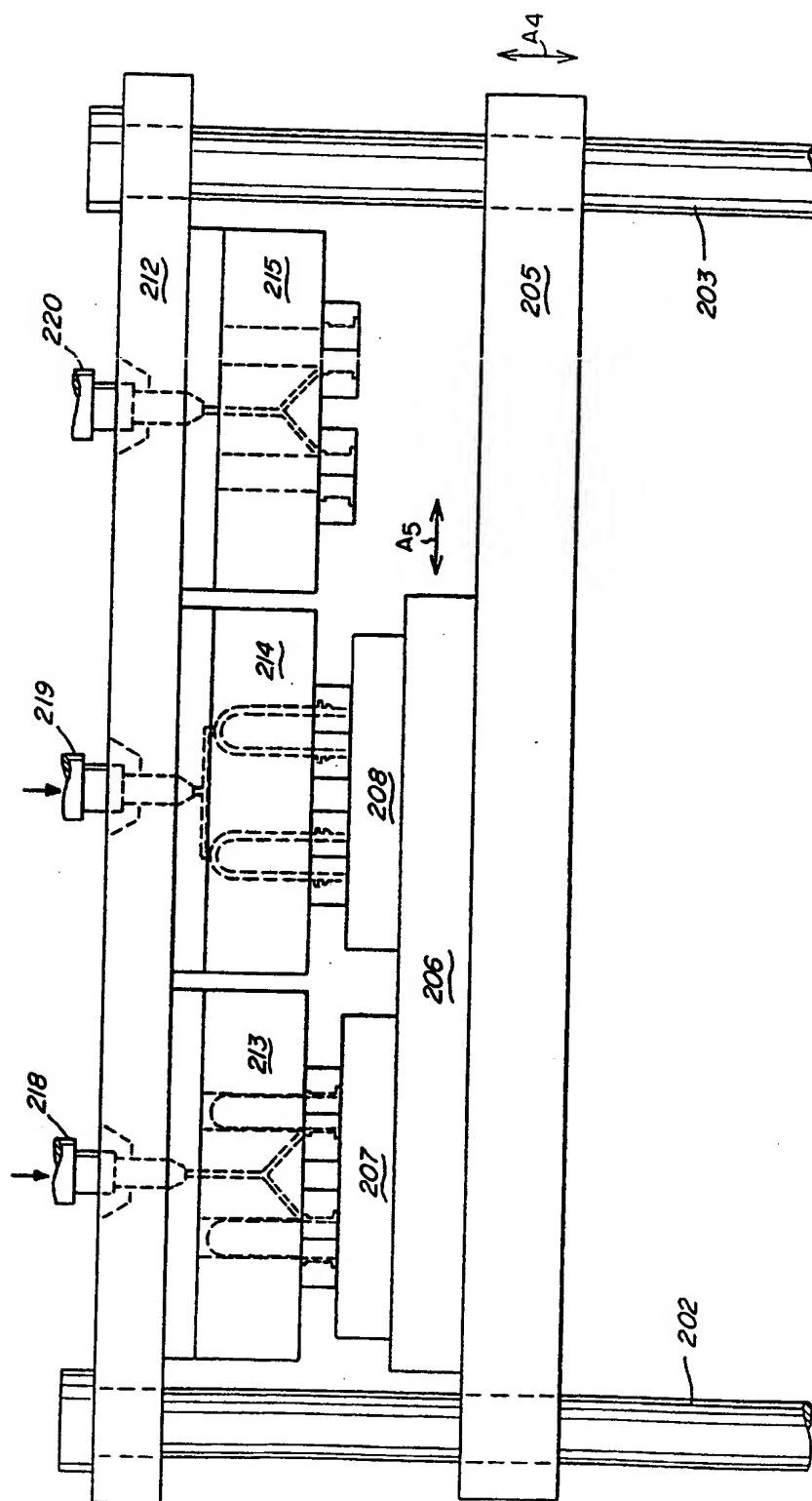


Fig. 6A

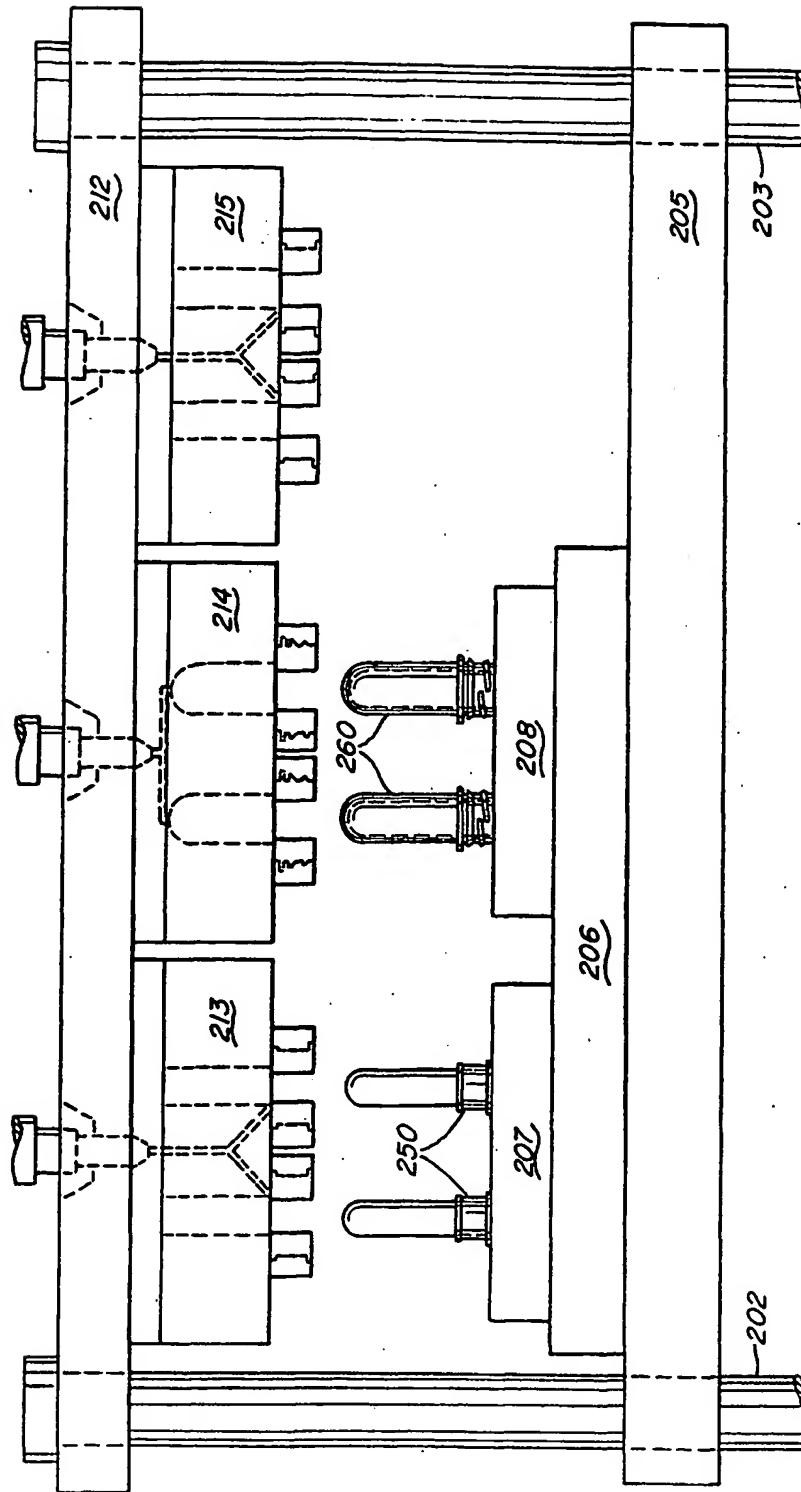


Fig. 6B

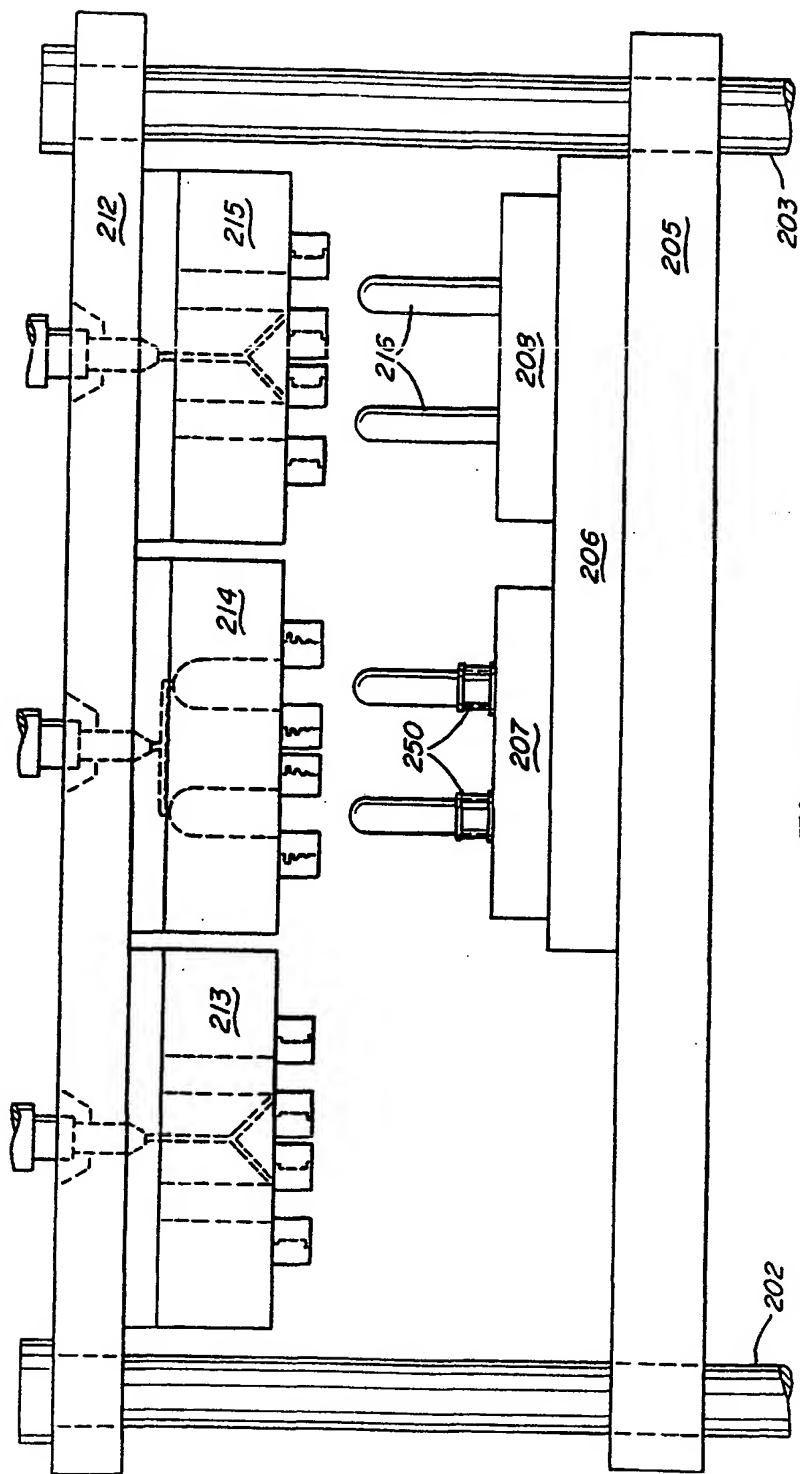
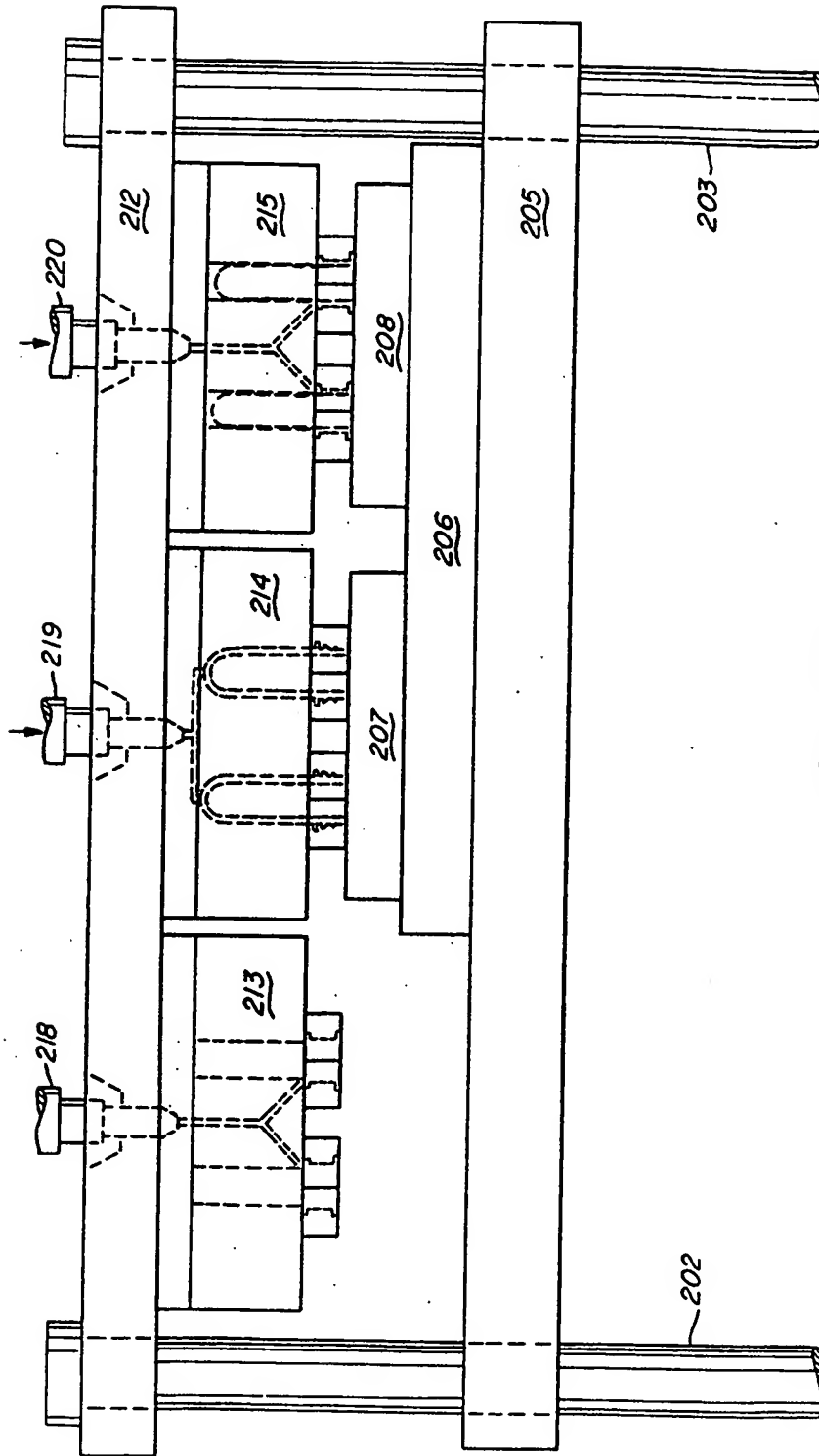


Fig. 6C



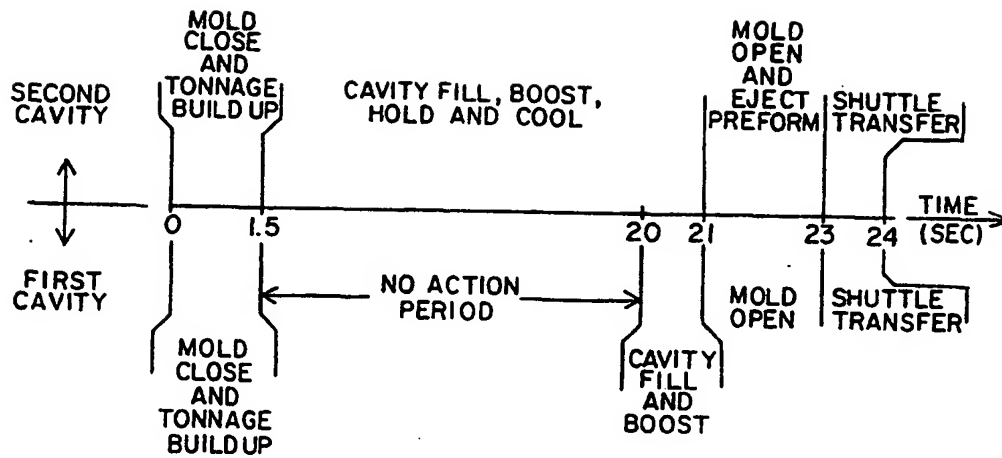


Fig. 7

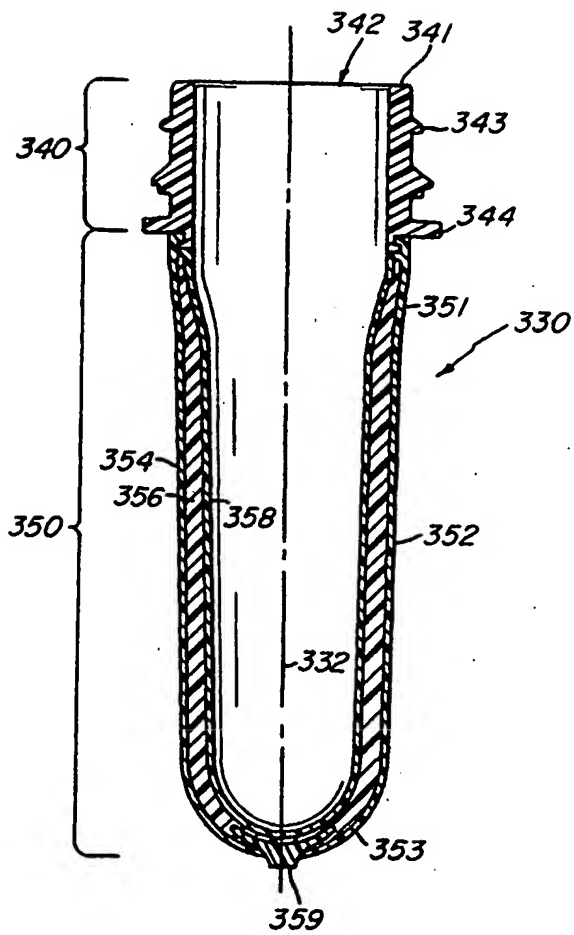


Fig. 8A

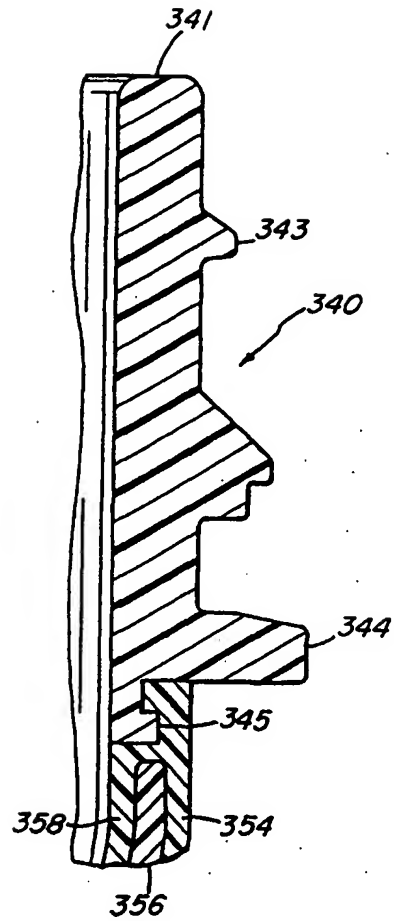


Fig. 8B

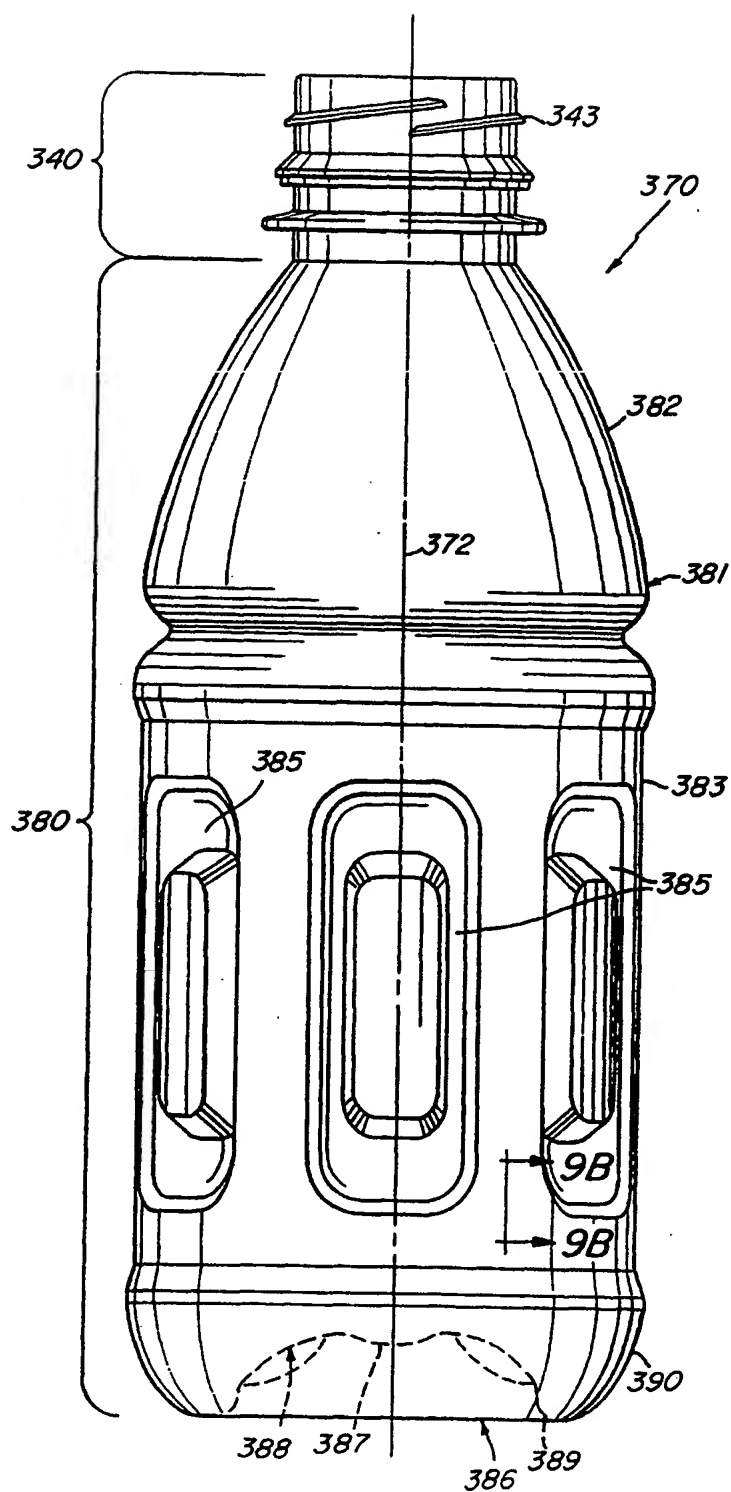


Fig. 9A

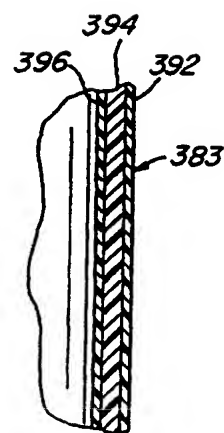


Fig. 9B

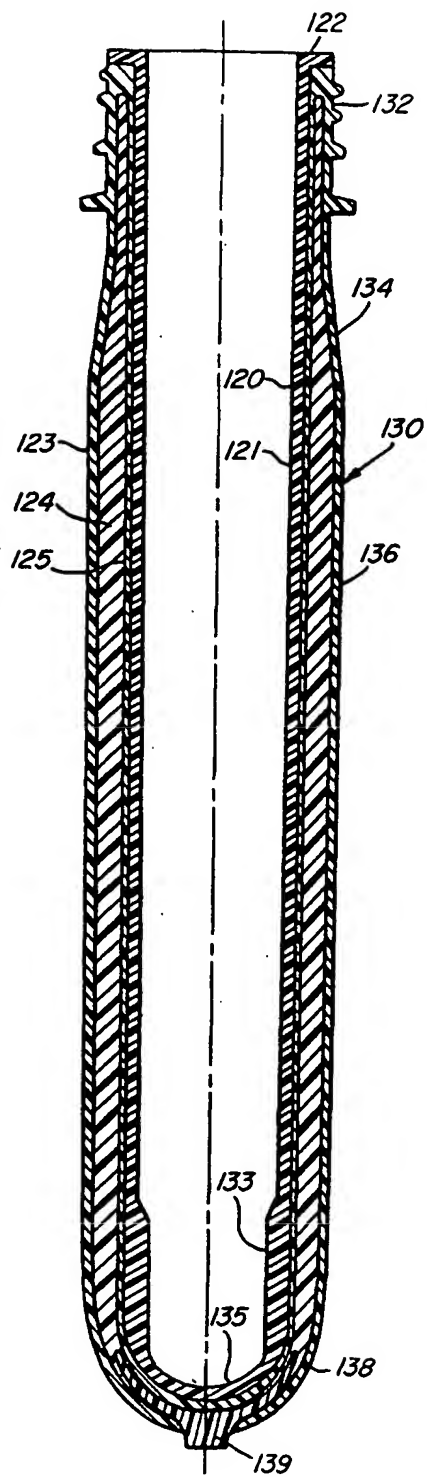


Fig. 10

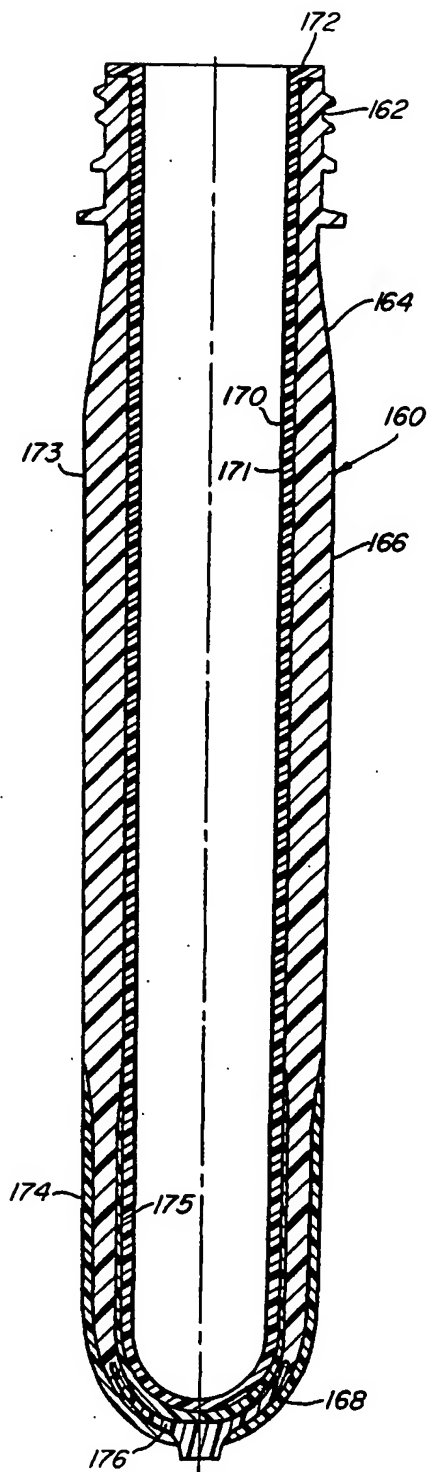


Fig. 11

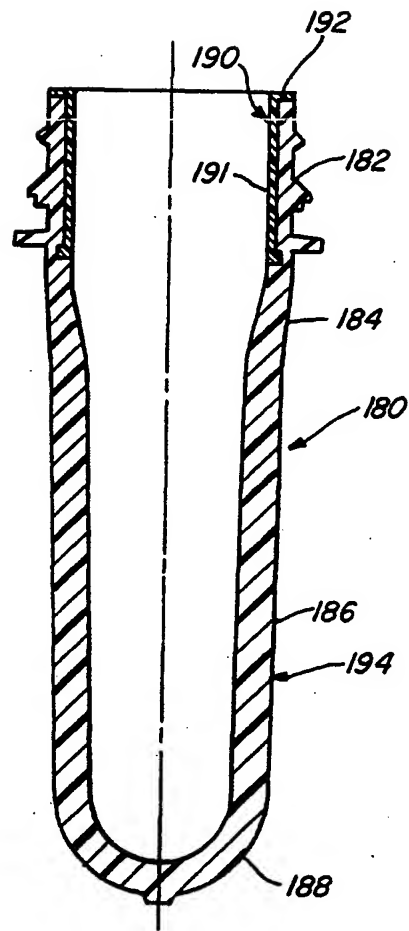


Fig. 12

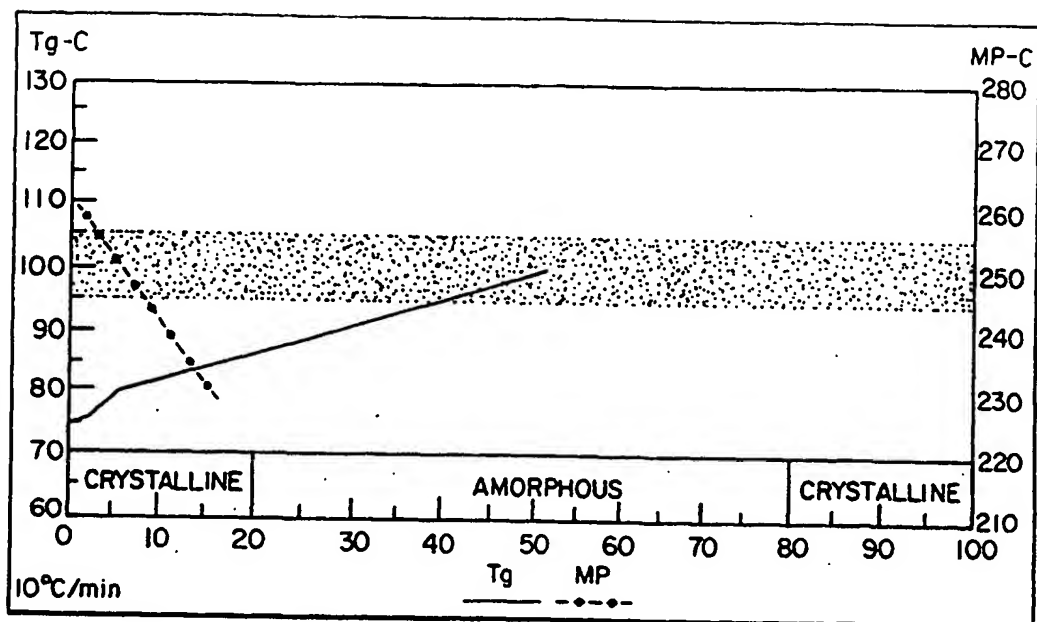


Fig. 13A

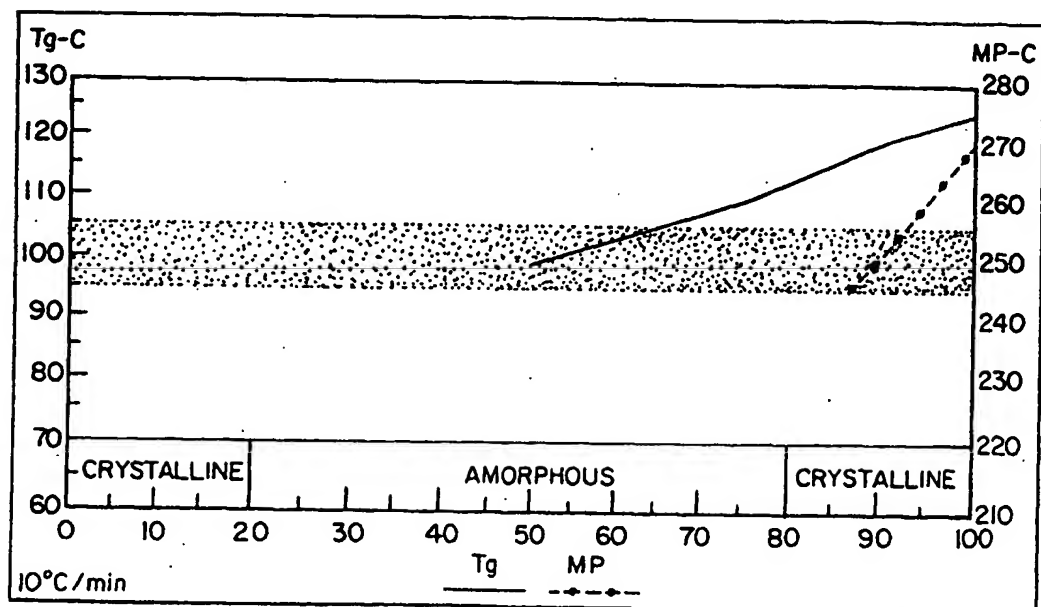


Fig. 13B

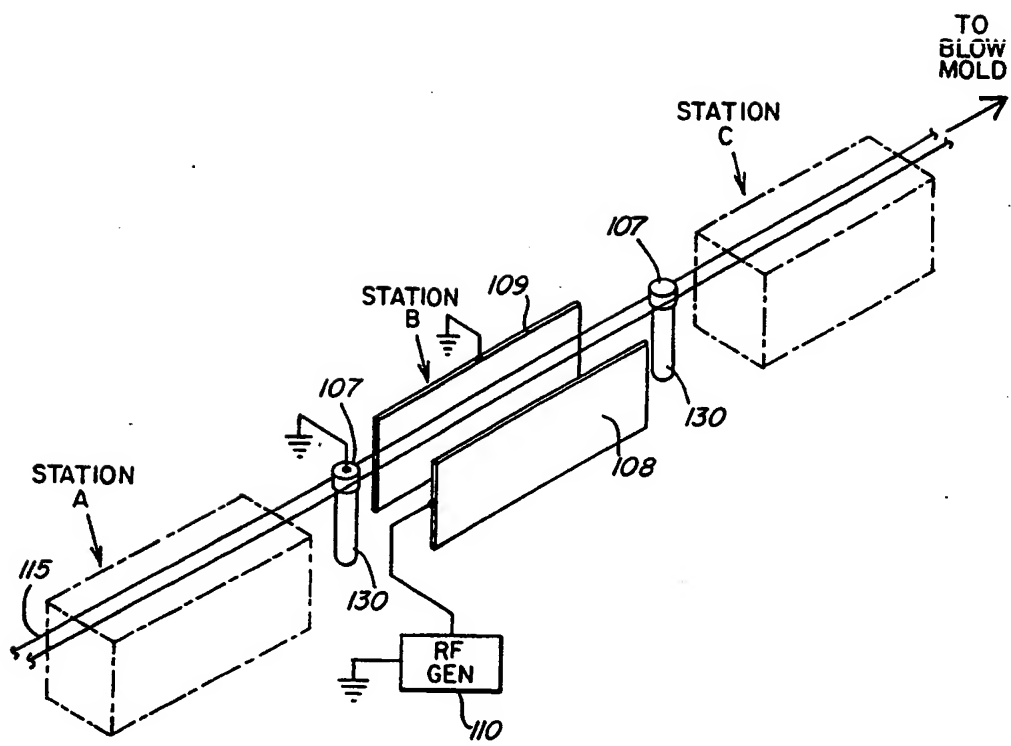


Fig. 14